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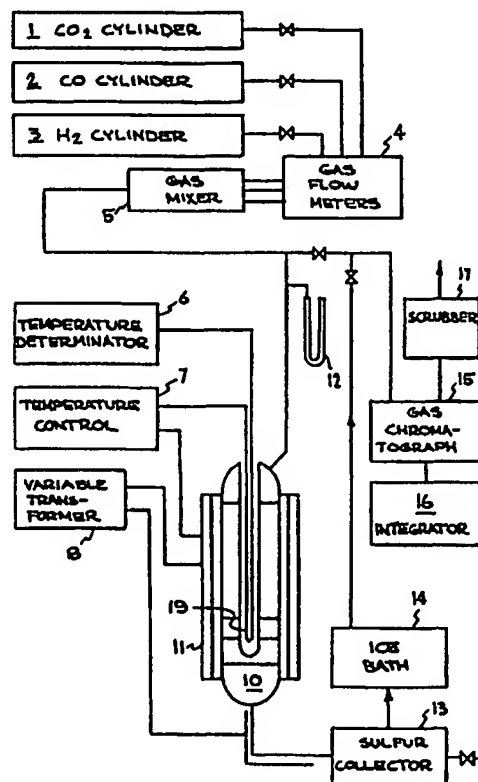
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(54) Title: SULFIDE CATALYSTS FOR REDUCING SO₂ TO ELEMENTAL SULFUR

(57) Abstract

A highly efficient sulfide catalyst for reducing sulfur dioxide to elemental sulfur, which maximizes the selectivity of elemental sulfur over byproducts and has a high conversion efficiency. Various feed stream contaminants, such as water vapor are well tolerated. Additionally, hydrogen, carbon monoxide, or hydrogen sulfides can be employed as the reducing gases while maintaining high conversion efficiency. This allows a much wider range of uses and higher level of feed stream contaminants than prior art catalysts.



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SULFIDE CATALYSTS FOR REDUCING SO₂ TO ELEMENTAL SULFUR

This invention was made with Government support under Contract No. DE-ACO3-76SF00098 between the U.S. Department of Energy and the University of California for the operation of Lawrence Berkeley National Laboratory. The Government has certain rights in this invention.

BACKGROUND OF THE INVENTION

This invention relates to catalysts which can convert sulfur dioxide to elemental sulfur, and the preparation method needed for their manufacture.

Industries Generating SO₂ A chronic concern for the environment has been release of pollution from industrial and other sources into the air and water. Of particular concern to environmentalists are gaseous emissions containing sulfur dioxide. When this gas rises to cloud level, the rain produced from these clouds can become highly acidic, at times reaching the acid levels of vinegar. Because the emissions and clouds effected by them can travel great distances beyond the point of initial emission, this form of pollution takes on international dimensions.

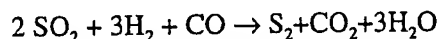
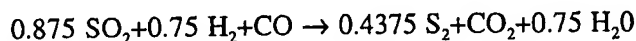
The effects of such industrially related acid rains are infamous. Streams and lakes in North Eastern America and Canada have been rendered devoid of their natural flora and fauna due to acidification by acid rain. Trees in these areas have also been badly compromised. Similar effects have been seen in Europe, where large sections of trees in the famous Black Forest have been damaged, and in some cases destroyed, by the effects of acid rain.

Flue gases emitted from burning sulfur-containing fossil fuels are the most common source of dilute sulfur dioxide (SO₂) containing industrial gases. Sulfur dioxide is the unwanted byproduct of a diverse array of industrial activities, such as coal-burning power plants, advanced integrated gasification combined cycle (IGCC) using hot gas clean up systems, petroleum sulfur plants tail gas treatment facilities, metallurgical operations, and the like. Because of regulatory constraints, these operations are currently hampered by a limited choice of available coal sources, working parameters, etc., in order to meet environmental regulatory mandates. Further reduction of SO₂ contaminants would allow longer operating times for these facilities while staying within the legally determined limits for emissions.

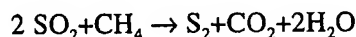
Regenerable flue gas desulfurization systems [FGD] and integrated gasification combined cycle [IGCC] hot gas cleanup systems have been developed for use in coal-based utility industries. These systems release a stream of high concentration [1%-30%] SO₂ gas. It is desirable to be able to convert the SO₂ gas to elemental sulfur using a single step process.

The petrochemical industry commonly uses the conventional Claus process for conversion of H_2S to elemental sulfur. This system releases a stream of tail gas containing SO_2 and H_2S . An additional tail gas treatment system is then required to reduce these residual gases to below 250 ppm in order to comply with environmental air regulations. Currently available tail gas treatment systems requiring an organic solvent absorption step are complex and expensive. The development of a new tail gas treatment process capable of reducing SO_2 by H_2/CO to elemental sulfur would be very desirable and cost effective.

Conversion of SO_2 to Elemental Sulfur Research efforts have been made to allow the conversion of sulfur dioxide to elemental sulfur. In these methods, sulfur dioxide is reduced with synthesis or natural gases. Synthesis gases are derived from coal ($\text{H}_2/\text{CO}=0.3\text{-}2.0$) or methane ($\text{H}_2/\text{CO}=3\text{-}5$). At elevated temperatures, sulfur dioxide can be converted to elemental sulfur through the following reactions:



Sulfur dioxide can be reduced with natural gas (mainly methane) as follows:



The reactions must be facilitated with catalysts in order to achieve a real time high conversion efficiency of SO_2 . Even with the assistance of numerous catalysts, commercially feasible conversion efficiencies have not been achieved.

In addition to elemental sulfur, the above reactions produce a number of undesirable byproducts. These can include hydrogen sulfide, carbonyl sulfide, carbon disulfide, and elemental carbon. These byproducts complicate the ability of the conversion reactions to effectively reduce the net airborne contaminants produced during industrial processing.

Because of the inadequacies of the above reactions when direct to industrial applications, research efforts have been carried out to bring this potentially useful area of technology to a level where it has practical applications. The thrust of these research efforts have been to improve the conversion efficiency of sulfur dioxide and increase the selectivity to the production of elemental sulfur at relatively low temperatures.

While there has been some success in this area of research, the results which have been reported to date can not practically be applied to commercial uses.

Oxide and Metal Catalysts Responding to the problems of current SO_2 capture methods, the catalyst research community has been attempting to develop regenerable flue gas desulfurization catalysts and processes. Most of the efforts to develop a practical SO_2 reductant catalyst have not progressed beyond basic research. However, recently certain researchers have reported more success.

Oxide and simple metal forms of metals represent the few SO₂ catalysts with appreciable activity. Many challenges have been encountered in this area of research, such as low yields, substantial reduction of sulfur yields by very low levels of water vapor, and unacceptable levels of unwanted byproducts.

By using syngas to reduce SO₂, Akhmedov et. al. [Azerb Khim. Zh(2), 95-9, 1983] developed several catalysts and obtained the following results: a 64-65% sulfur yield with a bauxite-bentonite catalyst at 350°C with a feed gas at a molar ratio (CO+H₂)/SO₂ of 2 and a space velocity of 1000 h⁻¹; a 82% sulfur yield with a NiO/Al₂O₃ catalyst at 300°C with a space velocity of 500 h⁻¹ [Zh. Prikl. Khim., 61(1), 16-20, 1988]; an 82% and 87.4% sulfur yield with a Co₃O₄/Al₂O₃ catalyst [Zh. Prikl. Khim., 61(8), 1891-4, 1988] at 300°C with a space velocity of 1000 h⁻¹ and 500 h⁻¹ respectively; a 82.3% and 78.6% sulfur yield with a NiO+Co₃O₄ catalyst [Khim. Prom. 1, 37-9, 1989] at 400°C with a space velocity of 500 h⁻¹ and 1000 h⁻¹ respectively. The development of a catalyst capable of obtaining better than 90% yield of sulfur with a high space velocity at low temperatures would be required to warrant a commercial application.

Natural gas or methane can also be used as reducing gases to recover elemental sulfur from SO₂. However, this process requires elevated temperatures, and typically produces undesirable byproducts such as hydrogen sulfide, carbonyl sulfide, carbon monoxide, and elemental carbon. A plant capable of producing 5 tons per day of elemental sulfur through the reduction of SO₂ by natural gas was developed and in operation in 1940 (Fleming et al, Industrial Engineering Chemistry Vol. 42, p2249, 1950). Because a secondary reactor was required to treat byproducts, this process was economically unattractive.

A more efficient process requiring two stages was developed to avoid some of the problems of the Fleming system. In the first step, part of the SO₂ was reduced to H₂S by methane and/or low value hydrocarbons. In the second step, the H₂S and the remaining SO₂ were converted to elemental sulfur in a multi-stage Claus unit [Bierbowere, et al Chemical Engineering Progress August, 1974].

Numerous research efforts have been made to develop a catalyst for sulfur dioxide reduction where the amount of byproducts produced is negligible, so that a second stage treatment will not be required. To date, none have been successful enough to warrant application to an industrial facility.

Flytzani-Stephanopoulos et al reported favorable results with mixed oxide catalysts in a limited environment, but rapidly decreasing sulfur yields in the presence of only one or two percent of water in the feed stream. In U.S. Patent 5,242,673 (issued 9/7/93) Flytzani-Stephanopoulos et al taught a cerium oxide catalyst which, in a dry environment with CO in stoichiometric amounts had better than 90% conversion rate (column 8, line 53-55), and in another case, a selectivity of sulfur dioxide toward elemental sulfur of 50-60% (column 9, lines 15-17).

In U.S. Patent No. 5,384,301, (issued 1/24/95) Flytzani-Stephanopoulos et al teach several new sulfur dioxide reducing oxide catalysts. $\text{CeO}_2(\text{La})$ showed a 95% conversion of SO_2 to elemental sulfur in a CO gas stream. With the addition of transition metals to produce $\text{Cu/CeI}_2\text{M}$, C/CeO_2 , and Ni/CeO_2 , the same level of conversion to sulfur was obtained. However, with only 2% H_2O in the gas stream, the conversion to sulfur dropped to 72%. These sulfur yields were also reflected in the $\text{Cu}_{0.15}\text{Ce}_{0.85}\text{O}_{1.85}$, $\text{Cu}_{0.026}\text{Pr}_{0.035}\text{Ce}_{0.65}\text{O}_{1.85}$, $\text{Gd}_2\text{Zr}_2\text{O}_7$, and $\text{Cu}_{0.15}(\text{Gd}_2\text{Zr}_2)_{0.8506.1}$ catalysts these researchers reported.

Sulfide Catalysts Sulfide forms SO_2 reductant catalysts have not been pursued by the catalyst research community beyond some very limited initial work due to the discouraging findings. Khalafalla et al found that when the iron on an iron-alumina catalyst was transformed to FeS , there was a decrease in activity, and in some cases showed no activity at all (Khalafalla et al. Journal of Catalysis vol. 24, pp. 121-129, 1972). Correlation of sulfidation with unwanted byproduct formation has also been reported (Haas et al., Journal of Catalysis vol. 29, pp 264-269, 1973). The present inventors have also developed sulfur dioxide reducing catalysts, as described in U.S. Patent No. 5,494,879 issued 2/27/96 and incorporated by reference herein.

A comparison of the oxide and sulfide forms of SO_2 catalysts is shown in the Comparison Chart below. The poor performance of the sulfide forms have led researchers to pursue the oxide forms of the catalysts.

SINGLE METAL SO₂ CATALYSTS COMPARING YIELDS FOR OXIDE AND SULFIDE FORMS

M ₂ *O ₃ /Al ₂ O ₃				M ₂ S ₃ Al ₂ O ₃		
Cat	t	Reductant	Y(S ₂)	t	Reductant	Y(S ₂)
	(°c)		(%)	(°c)		(%)
Cr*/Al ₂ O ₃	400	CO+H ₂	52.0 ^[2]	370	H ₂	24.2 ^[2]
Mo*/Al ₂ O ₃	450	H ₂	62.8 ^[1]	370	H ₂	49.1 ^[3]
Cu*/Al ₂ O ₃	400	CO+H ₂	35 ^[2]	370	H ₂	20.1 ^[3]
Co*/Al ₂ O ₃	400	CO+H ₂	70 ^[2]	370	H ₂	60.9 ^[3]
Ni*/Al ₂ O ₃	450	H ₂	61.7 ^[1]	370	H ₂	58.6 ^[3]

* M=Cr, Mo, Cu, Co, Ni;

^[1] Alkhazov et al Zh. Prikl. Zh. (J. Appl. Chem.) (9) 1826-31 (1991) (Russ)

^[2] M.M. Akhmedov et al Khim. Prom. (Chem. Ind.) [1] 37-9 (1989) (Russ)

^[3] Paik et al, Appl. Catal. B8 267-79 (1996).

It would be highly desirable to convert the many sources of sulfur dioxide from the many industrial activities that produce it to elemental sulfur. If this conversion could be accomplished in a commercially feasible manner, it would allow reclamation of sulfur and its recycling as a valuable chemical.

BRIEF DESCRIPTION OF THE INVENTION

The present inventive preparation process and the resulting unique catalysts provide unprecedented advantages over prior art sulfur dioxide reductant catalysts. The sulfide form of metals in the inventive catalysts provide unique advantages such as high yield of sulfur and low unwanted byproducts. This allows a single step conversion of SO₂ gas from industrial sources to elemental sulfur by simultaneously feeding a gas stream containing SO₂ and a separate stream of reducing gas through the inventive catalytic reactor.

The present invention is based on the unexpected discovery of the inventors that performance parameters of their prior oxide SO₂ reducing catalysts were substantially improved upon by employing sulfidation as a step in the preparation protocol. In one embodiment of the inventive process, surface metallic oxide species are converted to their sulfide forms by treatment with gases containing sulfur components. Another approach to producing the improved catalysts of the present invention is to introduce the sulfur components in the form of a solution, such as ammonium sulfide, during their manufacture.

Using any number of previous catalytic formulations as a starting point, the inventive sulfidation step taught in the present application results in new catalysts with unprecedented high

sulfur recovery rates. The inventive catalysts high efficiency remains even when hydrogen, carbon monoxide, or hydrogen sulfides are employed as the reducing gases.

Water vapor, a common poison of prior art catalysts, are well tolerated by the inventive catalyst, which shows no appreciable reduction in sulfur yields in their presence. The inventive catalysts work well at various pressures, and at a wide range of SO₂ concentrations [300 ppm to over 66.7%].

It is an object of the present invention to provide a sulfur dioxide reducing catalyst with a high conversion rate selectively to elemental sulfur.

It is another object of the invention to provide a sulfur dioxide reducing catalyst with a high conversion selectively to elemental sulfur that will be effective in coal burning power plants, advanced IGCC plants using hot gas treatment systems, petroleum sulfur tail gas treatment plants, and other industries which burn sulfur containing fuel or emit sulfur dioxide fumes.

It is yet another object of the present invention to provide an efficient sulfur dioxide reducing catalyst selective for elemental sulfur which can be operated in a wide range of temperatures and reducing gases, in the presence of water vapor, and at various pressures.

DETAILED DESCRIPTION OF THE INVENTION

The inventors have unexpectedly discovered a new class of catalysts that reduce sulfur dioxide to elemental sulfur, with dramatically improved critical qualities over prior art catalysts. This is accomplished by sulfiding a metallic salt impregnated support by either gas or solution sulfidation. The most important qualities which benefit from the present invention are high conversion efficiencies, specificity of conversion, and resistance to water poisoning. Thus, the inventors have produced a whole new class of catalysts which for the first time are capable of practical uses in industry.

The comparison chart above demonstrates the very unexpected nature of the inventors discovery. It compares several prior art oxide formulations with the same formulas in a sulfide form. The comparison shows that most sulfide forms have little function over a reasonable range of temperatures, and where they do show an activity, have poor or somewhat inferior characteristics to their oxide counterparts. In the face of these clear findings, the research communities could be discouraged for any serious experimental efforts into sulfide forms of sulfur dioxide reducing catalysts.

CATALYST PREPARATION STEPS

In its simplest form, the inventive catalysts are prepared by first impregnating a substrate with a solution of the metallic compounds, and then sulfiding these metals to form the final catalyst. Standard processing procedures such as drying and calcination are also employed. In two major embodiments of the invention, the sulfidation can be accomplished by gaseous treatment or by a sulfiding solution. When desired, these methods can be employed in combination.

Gaseous sulfidation converts the oxide forms of the metallic components to the sulfide form. When the solution sulfidation embodiment of the present invention is used, typically a nitrate form of the metallic components is chemically converted to the sulfide form by treatment by solutions such as ammonium sulfide in order to produce sulfide precipitates.

The compositions of the catalysts were analyzed using X-ray diffraction, BET surface area analysis, and atomic absorption elemental analysis. Gaseous treatment appears to produce a more surface sulfiding effect, while treatment with solutions accomplishes sulfidation of the inner portions of the substrate. Gaseous treatment also tends to provide a final product with some of the oxide form of the metals remaining, while treatment by solution results in a more complete conversion to sulfide forms.

Oxygen Free Environment To avoid the reintroduction of the oxide form of the metallic components to the catalyst, the preparation steps enumerated below which take place during or after the sulfiding step must be accomplished in an oxygen limited environment. By example the impregnation step generally can take place in a standard gaseous environment.

Typical, the gaseous stream used to exclude oxygen in the relevant steps is nitrogen, argon, helium, or other inert gas or gas combination. These flow-through stream conveniently serve both to deliver the sulfidation gas stream to the impregnated substrate in the case of gaseous treatment, and to draw unwanted byproducts away from the developing catalyst.

Metal Solution Impregnation of Substrate A common first step in the various embodiment of the inventive preparation method is the impregnation of a substrate, typically alumina, with a solution of the metal salt or metal salts which will make up the final formulation. Metal salts of the desired formulation are first dissolved in water or other appropriate solvents or solvent combinations. While the metal salts are typically in nitrate form, they can also be less preferred metal carbonates or nitrites.

The solution carrying the metallic components is then used to impregnate the alumina substrate with the various metal components of the desired formulation. The metal salt solution impregnation step can be accomplished in an ambient gas environment. The impregnated substrate is then evaporated to dryness.

When the various metal salts have compatible solubilization parameters, they are placed in solution in one step. Those metal salts that do not have compatible solubilization parameters, such as molybdenum, must be impregnated into the substrate and dried sequentially, as described below.

The alumina substrate used in the present invention can be of virtually any type, such as α alumina, β alumina, or γ alumina. The latter is employed in the examples set forth below. Because of the ease of processing available in the present invention, the substrate can be in a wide range of γ forms, such as plates, granules, extrusions, pellets, honeycomb, monoliths, etc.

In some cases, such as with a molybdenum component, the solution parameters exceed those of more standard metal components, and would cause premature precipitation and other difficulties if combined together. In such cases, the carrier can be impregnated sequentially with the incompatible solvents. By example, molybdenum is typically soluble at a much more basic pH than is compatible with other metallic nitrates. Therefore, molybdenum would be introduced on the substrate only after treatment with the other metal nitrates, including the drying steps.

Evaporation of Solution The dissolved metal nitrates are then admixed with the alumina substrate, and the solution evaporated. This step can also occur in an ambient gas environment. The evaporation of the solution can be accomplished by any number of conventional means, such as by vacuum, gentle heating, or simply leaving the solution open to evaporation. One standard means, gentle heating, can take place at under about 200°C. At preferred range of evaporation temperatures are from 100°C to 150°C. This heating also serves to evaporate crystalline water.

SULFIDATION BY GASEOUS TREATMENT

In one embodiment of the present invention, the dried, metal compound impregnated substrate described above is sulfidated by gaseous treatment. X ray diffraction studies appear to indicate that in this embodiment of the inventive preparation method the sulfide components are most concentrated at the surface of the substrate, but the metallic component in the deeper layers of the substrate seem to maintain their oxide form. The active surface of the catalyst includes all areas of the catalyst which come in contact with the reactant, and which are activity catalyzing SO₂ into elemental sulfur. This typically includes the surfaces of porous areas.

As a first step in the inventive preparation method using sulfidation by gaseous treatment, the impregnation of a substrate and drying are accomplished as above. This impregnated, dried substrate serves as the precursor to the final gas sulfided catalyst.

Removal of Crystalline Water After the drying step, the impregnated is treated at a higher temperature in part to assure a more complete removal of water which was not eliminated during the drying step. The treatment typically is given for 15 minutes to four hours, depending on such parameters as the size of material to be treated, and the temperature of treatment. A preferred time is about a half an hour. The temperature of treatment can range from 200°C to 300°C, with the preferred temperature at about 250°C.

Decomposing of Nitrate The dried impregnated substrate is then treated at a third higher temperature level. When the metals in solution are introduced in the form of nitrates, this step serves to decompose their nitrate component. The nitrate component is usefully decomposed and potential nitrate contaminants reduced.

Typically, the nitrate decomposition temperature is at 300°C to 450°C, with a preferred temperature of around 400°C. The treatment can take place from 15 minutes to 6 hours, depending on the size of the precursor catalyst, the temperature employed, the feed stream speed, etc.

This step further decomposes remaining nitrate components and serve to more completely decompose nitrate and vaporize NO₂. These vaporized materials are eliminated by the feed stream. Exemplifying the effects of this step is;



Calcination of Impregnated Substrate Once the metal components have been dried on the surface of the alumina, the impregnated alumina is calcinated. This results in changes to the structure of the catalyst components.

The final, highest level of heat treatment is the calcination step, which results in the formation of a metal oxide complex of the various components, rather than a standard alloy. Calcination can be accomplished at temperatures from 500°C to 700°C. Depending on the selected temperature, the calcination step can be accomplished in from 2 hours to 2 days. A preferred treatment would be at 600°C for 4 hours. The calcination temperature is in part determined by the structural limitations of the substrate. After calcination, the impregnated substrate is typically allowed to cool to room temperature in order to move the materials to a second vessel. However, when the same vessel is used for sulfiding, the cooling step is not necessary.

Gaseous Sulfiding of Impregnated, Calcinated Precursor Catalyst The calcinated product described above is then treated at a higher temperature by a sulfur containing gaseous stream. This treatment by gas converts (the metals near or on the surface of the monolith from the oxide to the sulfide form.) For this reason, the steps up to this point in the gaseous sulfidation process need not be carried out in an oxygen free environment. Sulfidation takes place under an oxygen free environment.

The sulfiding of the calcinated precursor catalyst by gas has several parameters, all of which serve to balance the various choices when selecting the others. This provides great flexibility in processing techniques, and allows industry to specifically optimize the process for particular substrates or catalyst formulations, and for temperatures, gas stream flow rates and concentrations, etc. which are the most economical.

Typically, the sulfiding continues until the catalyst precursor is saturated. This point can be judged as completed when the gaseous treatment stream has the same concentration of the sulfur component both before and after flowing over the catalyst precursor. Partial sulfiding can also been provided if certain mixed sulfide/oxide surface formulations having advantageous qualities are required.

The various parameters for the gas sulfiding process are mutually determinant. For instance, if high temperatures are used, sulfidation can be accomplished very quickly. Low gaseous flow rate or low sulfide content of the treatment stream can be compensated for by treating a small amount of precursor catalyst over a longer period of time.

The range of temperatures available to effectively accomplish sulfidation of the precursor catalyst are broad. Selection of treatment temperature will take into account such factors as cost, ease of processing, and substrate stability. Effective sulfidation temperatures can typically range from 200°C to 700°C. A more preferred range for sulfidation temperatures is from 350°C to 650°C. The most preferred range is from 500°C to 620°C.

The time needed for effective sulfidation treatment is also flexible. For instance, with a good flow rate and high SO₂ concentration, effective treatment can take as little as 10 minutes. On the other hand, if only a low feed rate and temperature is available, or to provide gentle treatment parameters, a treatment time of five days or more can be provided. A more typical range of treatment time would be 30 minutes to 24 hours. A most preferred range of treatment time is about an hour.

A wide range of treating gas concentrations can be used to sulfide the catalyst precursor. These can range from 0.1% to 100%. Very concentrated treating gas is particularly useful when treating a large amount of catalyst precursor over a reasonable time period. When low concentration treating gas is available, longer time and higher temperature of processing is required. A preferred range of treating gas concentration is 5%-40%. The most preferred range is 10%.

The gases used to treat the catalyst precursor can be of any number of formulations. For instance sulfur dioxide in a methane stream [SO₂/CH₄], sulfur dioxide in a hydrogen stream [SO₂/H₂], or sulfur dioxide in a carbon monoxide stream [SO₂/CO]. The various non-sulfur dioxide materials listed above can also be used in combination as a reductant for the sulfur dioxide component to produce the gaseous sulfides, H₂S and/or COS for sulfidation of metal oxides. Thus, one could have an effective treatment stream in the present invention which would include varying levels of methane, hydrogen, and carbon monoxide with the desired percentages of sulfur dioxide. Other gaseous sources of sulfides can also be used directly, such as H₂S and/or COS, by themselves or in combination with the gases described above.

An example of the gaseous sulfiding preparation is the sulfidation of Fe₄Co₁Ni₁Mo₁Pr₆Mn₂O_{26.33}/γ-Al₂O₃. A fresh H₂S gas can be used for the sulfidation. Fe₄Co₂Ni₂Mo₁Mn₂O_{17.66}/γ-Al₂O₃ oxide catalyst is reacted with H₂S at 620°C for between 0.5 and 4 hours. Lower temperatures are also workable when H₂S is employed. An example is the preparation of Bi₂O₃S_y/γ-Al₂O₃ from the reaction of oxide catalyst with H₂S at 300°C for an extensive period (24 hours). The performance of this catalyst is shown in Table 1.

SULFIDATION BY TREATMENT WITH SOLUTION

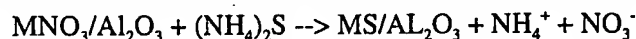
A second major embodiment of the inventive catalyst production method is sulfidation by treatment of the impregnated catalyst precursor with a sulfiding solution. This method results in a

more uniform deposition of the sulfide form of the catalytic metals through the final catalyst, rather than a more surface effect as seen in the gaseous treatment method described above. Another important feature of the solution method is that sulfidation appears to be much closer to full completion; there is a lower amount of remaining oxide form as compared to the gaseous treatment method. The active surface of the catalyst includes all areas of the catalyst which come in contact with the reactant, and which are activity catalyzing SO_2 into elemental sulfur. This typically includes the surfaces of porous areas.

In the solution sulfidation method, the evaporated metal nitrates impregnated substrate is treated by a sulfiding solution after the impregnation and drying steps described above. The sulfiding solution treated substrate is then heated at four different levels. Each temperature level serves to promote the development of the catalyst, often partially accomplishing some of the purposes of the others. However, there is a tendency for a certain specialized effect to take place in each of the different levels.

At the first, lowest temperature, a simple drying of the solution carrier is accomplished. The next highest temperature treatment serves to remove crystalline water. The third yet higher temperature acts to decompose ammonium nitrate and sulfide to vaporize other unwanted potential contaminating materials. The final, highest temperature acts as a calcination step, which forms the final catalytically active metal complex product.

Solution Sulfidation Various solutions can be employed to convert the nitrate forms of the precursor catalyst to the sulfide form. Typical, an ammonium sulfide solution is used. The ammonium sulfide solution is introduced in stoichiometric proportions to the metallic components, with an excess, typically 10%, in order to ensure complete conversion:



The sulfidation solution can be prepared at concentrations which are most convenient for the production effort. Ranges from 5% to 30% concentration will, among others, be useful in the present invention. A standard laboratory concentration is around 10%. The sulfidation solution, which can be combined with the metal solution first, is simply admixed directly with the precursor treated substrate.

Drying Step This second drying step in this case typically includes heating, and is distinct from the initial drying step of the original metal salt impregnated substrate. The sulfided solution treated impregnated substrate is dried at from 50°C-100°C. Virtually all of the surface water and other solution liquid is removed in this step, as is much of the deeper water, such as that in the pores and close to the surface. The drying step serves to release to some degree potentially contaminating nitrogen components and water in a gaseous state.

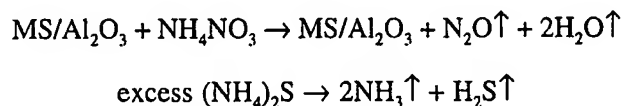
It is at this point that additional impregnation and sulfiding steps are taken where metallic salts with incompatible solution criteria are to be included in the formulation. A typical metallic component of this kind would be molybdenum. The additional impregnation and sulfiding steps are described in the example section below, and in the equation above.

Removal of Crystalline Water After the drying step, the impregnated is treated at a higher temperature in part to assure a more complete removal of water which was not eliminated during the drying step. The treatment typically is given for 15 minutes to four hours, depending on such parameters as the size of material to be treated, and the temperature of treatment. A preferred time is about a half an hour. The temperature of treatment can range from 200°C to 300°C, with the preferred temperature at about 250°C.

Decomposing of Nitrate and Sulfide The dried impregnated substrate is then treated at a third higher temperature level. When the metals in solution are introduced in the form of nitrates, this step serves to decompose ammonium nitrate and sulfide components. The ammonium nitrate and sulfide components are decomposed and potential contaminants reduced.

Typically, the nitrate decomposition temperature is at 350°C to 450°C, with a preferred temperature of around 400°C. The treatment can take place from 15 minutes to 6 hours, depending on the size of the precursor catalyst, the temperature employed, the feed stream speed, etc.

This step further decomposes remaining nitrate components and serve to more completely vaporize NO₂, NH₃, and H₂S potential contaminants. These vaporized materials are then eliminated by the feed stream. Exemplifying the effects of this step is;



Calcination The final, highest level of heat treatment is the calcination step, which the inventors hypothesize results in the formation of a metal sulfide complex of the various components, rather than a standard alloy. Calcination can be accomplished at temperatures from 500°C to 700°C in the absence of oxygen. Depending on the selected temperature, the calcination step can be accomplished in from 2 hours to 2 days. A preferred treatment would be at 620°C for 4 hours.

INVENTIVE CATALYST PERFORMANCE

Testing Equipment and Parameters Experiments were carried out between 200°C and 820°C. The space velocity ranged from 1,000 h⁻¹ to 15,000 h⁻¹. The molar ratio of the sum of H₂ and CO to SO₂ ranged from 1.4 to 3.0, while the molar ratio of H₂ to CO varied from 0.3 to 5 to cover the entire composition range of synthesis gas produced from different types of coal and from methane.

A schematic flow diagram of the apparatus is shown in Diagram 1. The experimental setup consists of three separate sections: the gas supply section, the main reactor, and the detection and analysis section. Gases are supplied from compressed gas cylinders (Matheson Gas Products) to

gas flow meters before entering a gas mixer. Two sizes of the tubular reactors are used in the experiments. The smaller one is fabricated from a 1.2-cm-o.d. with a 1-mm wall thickness quartz tube. The larger one is from a 2.5-cm-o.d. with a 1-mm wall thickness quartz tube. The entire reactor is mounted inside a tubular furnace.

The smaller reactor is 7 cm long, while the larger reactor is 17 cm long. The reactors consist of three zones. The inlet or the preheating zone (2.5 cm long) is packed with 20 mesh quartz chips, the reaction zone is packed with catalysts (either 30-40 sieve particles or 3 mm diameter by 5 mm height granules), and the outlet zone (1 cm) is packed with quartz chips (20 mesh), mainly for the purpose of supporting the catalyst, which sat on a perforated quartz plate having seven holes for gas exit. A thermocouple, reaching the center of the catalytic packing, provide measurement of the temperature of catalytic reactions.

After the last section of the reactor, the gases pass through a sulfur collector at room temperatures, and then enter into an on-line trap cooled in an ice bath to condense water before entering a six-port sampling valve which is used to inject the products of the catalytic reactions into the gas chromatograph. Finally, the exit gases pass into a scrubber containing concentrated NaOH.

The inlet and exit gases are analyzed by using a gas chromatograph equipped with a column switching valve and a thermal conductivity detector. A 4-meter Porapak P (60-80 mesh) column was employed at 90°C (100 mA) for the analysis of SO₂, H₂S, COS, H₂O, and N₂. Another 4-meter column with Molecular sieve 13X at room temperature was used for the analysis of H₂, CO, and O₂. The carrier gas is helium.

Calculations and Definitions The catalytic conversion of SO₂ to elemental sulfur by synthesis gases or methane may produce unwanted side products such as H₂S, COS, and CS₂. The success of a process for the reduction of SO₂ will partly depend on the development of a catalyst which will maximize the selectivity of elemental sulfur over side byproducts. The conversion efficiency of SO₂, the yield of the side products, and the selectivity of elemental sulfur were evaluated for different formulations of catalysts.

The conversion (%) of SO₂ (C) is calculated by;

$$C = 100 (F^i_{SO_2} - F^o_{SO_2}) / F^i_{SO_2}$$

while, $F^i_{SO_2}$ is the flow rate (ml/h) of input SO₂, and $F^o_{SO_2}$ is the flow rate of output SO₂.

The yield (%) of hydrogen sulfide (Y_{H₂S}), carbonyl sulfide (Y_{COS}), and elemental sulfur (Y_{S₂}) is respectively calculated by

$$Y_{H_2S} = 100 F_{H_2S} / F^i_{SO_2} ,$$

$$Y_{COS} = 100 F_{COS} / F^i_{SO_2} , \text{ and}$$

$$Y_{S_2} = C - Y_{H_2S} - Y_{COS}$$

while, F_{H_2S} and F_{COS} are the flow rate (ml/h) of H₂S and COS output respectively.

The selectivity (%) of elemental sulfur (SS_2) is calculated by

$$SS_2 = Y_{S_2} / (Y_{S_2} + Y_{H_2S} + Y_{COS})$$

The space velocity (S.V.) is defined as

$$S.V. = F_{Total} / V_{cat} \text{ (h}^{-1}\text{)}$$

while, F_{Total} is the sum of the flow rates (ml/h) of all input gases, i.e. $F_{Total} = F_{SO_2} + F_{CO} + F_{H_2}$, and V_{cat} is the volume (ml) of the catalyst.

PERFORMANCE RESULTS

I. LOW SO_2 LEVELS.

The following tests were done at low (0.29% -3.37%) SO_2 concentrations in the feed stock with various catalytic formulations. These conditions reflect aspects of Claus reaction tail gas treatment and power plant flue gas treatment. Formulations evaluated include transition metals, combinations of transition metals and rare earth metals, combinations of transition metals with other active metal components, alkaline and alkaline earth metals.

The SO_2 concentrations generally ranged between 0.29% and 3.37%. It was demonstrated that the inventive catalysts were very effective for the conversion of low concentrations of SO_2 to elemental sulfur. It was also demonstrated that syngas and H_2S can be effectively used as reductants for the reduction of SO_2 to elemental sulfur.

A. Transition Metal Formulations

The following four examples show the performance of transition metal formulations at low SO_2 concentrations. The first three use syngas, while the fourth employs H_2S as a reductant:

1. The reduction of 0.3% SO_2 with a syngas [$(H_2/CO)=3$] over a catalyst comprised of $Fe_4Co_2Ni_2Mo_1Mn_2O_{17.66-y}Sy$ supported on $\gamma-Al_2O_3$. The molar ratio of syngas to SO_2 in the feed gas stream was 2, i.e. [$\{(3H_2+CO)/SO_2\}=2$]. The catalyst weighs 10 gr. A sulfur yield of 78.7% was obtained at 640°C. (Table 1)

2. The reduction of 0.3% SO_2 with a syngas [$(H_2/CO)=3$] over a catalyst comprised of $Fe_4Co_2Ni_2Mo_1Mn_2O_{17.66-y}Sy$ supported on $\gamma-Al_2O_3$. The molar ratio of syngas to SO_2 in the feed gas stream was 5.33, i.e. [$\{(3H_2+CO)/SO_2\}=5.33$]. The catalyst weighs 10 gr. A sulfur yield of 92.6% was obtained at 420°C. (Table 2)

3. The reduction of 0.3% SO_2 with a syngas [$(H_2/CO)=3$] over a catalyst comprised of $Fe_4Co_2Ni_2Mo_1Mn_2O_{17.66-y}Sy$ supported on $\gamma-Al_2O_3$. The molar ratio of syngas to SO_2 in the feed gas stream was 8, i.e. [$\{(3H_2+CO)/SO_2\}=8$]. The catalyst weighs 10 gr. A sulfur yield of 90% was obtained at 440°C. (Table 3)

4. The reduction of SO_2 with H_2S over a catalyst comprised of $\text{Fe}_4\text{Co}_2\text{Ni}_2\text{Mo}_1\text{Mn}_2\text{S}_{17.66}$ supported on $\gamma\text{-Al}_2\text{O}_3$. The molar ratio of H_2S to SO_2 in the feed gas stream was 2. The catalyst weighs 10 gr. Sulfur yields of 92.3% and 90.2% were obtained with a feed gas SO_2 concentration of 3.37% (at 240°) and 0.92% (at 200°C), respectively. (Table 4 a, b, c)

B. Combined Transition Metal with Rare Earth Metal Formulations

The following test provides characteristics of combined transition metal with rare earth metal formulations, using syngas as a reductant, with 0.3% SO_2 in the feed stock:

1. The reduction of 0.3% SO_2 with a syngas $[(\text{H}_2/\text{CO})=3]$ over a catalyst comprised of $\text{Fe}_4\text{Co}_1\text{Ni}_1\text{Mo}_1\text{Pr}_6\text{Mn}_2\text{O}_{26.33}\text{-ySy}$ supported on $\gamma\text{-Al}_2\text{O}_3$. The molar ratio of syngas to SO_2 in the feed gas stream was 8, i.e. $[(3\text{H}_2+\text{CO})/\text{SO}_2]=8$. The catalyst weighs 10 gr. A sulfur yield of 90.5% was obtained at 620°C . (Table 5)

C. Combined Transition Metal with Other Active Metal Formulations

The following four examples provide characteristics of inventive catalysts incorporating other active metal components with low SO_2 concentrations in the feed stock.

1. The reduction of 0.3% SO_2 with a syngas $[(\text{H}_2/\text{CO})=3]$ over a catalyst comprised of $\text{Fe}_1\text{Co}_1\text{Ni}_1\text{Bi}_5\text{Cu}_5\text{O}_{16.33}\text{-ySy}$ supported on $\gamma\text{-Al}_2\text{O}_3$. The molar ratio of syngas to SO_2 in the feed gas stream was 8, i.e. $[(3\text{H}_2+\text{CO})/\text{SO}_2]=8$. The catalyst weighs 10 gr. A sulfur yield of 92% was obtained at 620°C . (Table 6)

2. The reduction of 0.3% SO_2 with a syngas $[(\text{H}_2/\text{CO})=3]$ over a catalyst comprised of $\text{Bi}_1\text{Cu}_1\text{O}_{2.5}\text{-ySy}$ supported on $\gamma\text{-Al}_2\text{O}_3$. The molar ratio of syngas to SO_2 in the feed gas stream was 2, i.e. $[(3\text{H}_2+\text{CO})/\text{SO}_2]=2$. The catalyst weighs 10 gr. A sulfur yield of 90.9% was obtained at 600°C . (Table 7)

3. The reduction of 0.3% SO_2 with a syngas $[(\text{H}_2/\text{CO})=3]$ over a catalyst comprised of $\text{Bi}_2\text{O}_3\text{-ySy}$ supported on $\gamma\text{-Al}_2\text{O}_3$. The molar ratio of syngas to SO_2 in the feed gas stream was 8, i.e. $[(3\text{H}_2+\text{CO})/\text{SO}_2]=8$. The catalyst weighs 10 gr. The results show that a sulfur yield of 92.8% was obtained at 600°C . (Table 8)

4. The reduction of 0.3% SO_2 with a syngas $[(\text{H}_2/\text{CO})=3]$ over a catalyst comprised of Bi_2S_3 supported on $\gamma\text{-Al}_2\text{O}_3$. The molar ratio of syngas to SO_2 in the feed gas stream was 5.33, i.e. $[(3\text{H}_2+\text{CO})/\text{SO}_2]=5.33$. The catalyst weighs 10 gr. The results show that a sulfur yield of 93% was obtained at 600°C . (Table 9)

D. Alkaline and Alkaline Earth Metal Formulations

The following five tests provide characteristics of inventive catalysts incorporating alkaline metals with low SO₂ concentrations in the feed stock. The first four examples use syngas, while the fifth employs H₂S as a reductant for the conversion of SO₂ to elemental sulfur:

1. The reduction of 0.3% SO₂ with a syngas [(H₂/CO)=3] over a catalyst comprised of Li₂O_{1-y}Sy supported on γ -Al₂O₃. The molar ratio of syngas to SO₂ in the feed gas stream was 2, i.e. [(3H₂+CO)/SO₂]=2]. The catalyst weighs 10 gr. A sulfur yield of 90.6% was obtained at 600°C. (Table 10)

2. The reduction of 0.3% SO₂ with a syngas [(H₂/CO)=3] over a catalyst comprised of Na₂O_{1-y}Sy supported on γ -Al₂O₃. The molar ratio of syngas to SO₂ in the feed gas stream was 2.66, i.e. [(3H₂+CO)/SO₂]=2.66]. The catalyst weighs 10 gr. A sulfur yield of 95.2% was obtained at 440°C. (Table 11)

3. The reduction of 0.3% SO₂ with a syngas [(H₂/CO)=3] over a catalyst comprised of K₂O_{1-y}Sy supported on γ -Al₂O₃. The molar ratio of syngas to SO₂ in the feed gas stream was 2, i.e. [(3H₂+CO)/SO₂]=2]. The catalyst weighs 10 gr. A sulfur yield of 91.9% was obtained at 600°C. (Table 12)

4. The reduction of 0.3% SO₂ with a syngas [(H₂/CO)=3] over a catalyst comprised of Cs₂O_{1-y}Sy supported on γ -Al₂O₃. The molar ratio of syngas to SO₂ in the feed gas stream was 2, i.e. [(3H₂+CO)/SO₂]=2]. The catalyst weighs 10 gr. A sulfur yield of 92% was obtained at 620°C. (Table 13)

5. The reduction of SO₂ with H₂S over a catalyst comprised of Na₂S supported on γ -Al₂O₃. The molar ratio of H₂S to SO₂ in the feed gas stream was 2. The catalyst weighs 10 gr. Sulfur yields of 92.2%, 92.2%, and 92.9% were obtained at 220°C with SO₂ concentrations of 0.29%, 0.92%, and 3.37%, respectively. (Table 14 a, b, and c)

II. HIGH SO₂ LEVELS

The following tests show the capabilities of the inventive catalysts with high SO₂ concentration in the feed stock, that is at 5%, 33.3%, and 66.6%. These conditions are similar to those from Hot Gas Cleanup Systems employed in Advanced Integrated Gasification Combined Cycle (IGCC) Power Plants and from regenerable SO₂ scrubbers. The following formulations were evaluated: transition metal, combined transition metal with rare earth metal, combined transition metal with other active metal, and noble metals. It was also demonstrated that methane,

carbon monoxide, and/or syngas can all be effectively used as reductants for the reduction of SO₂ to elemental sulfur.

A. Transition Metal Formulations

The following two examples show the performance of transition metal formulations using methane as a reductant with high SO₂ concentrations in the feed stock. The effect of support materials for the catalysts were evaluated in the second example.

1. The reduction of 66.6% SO₂ with methane over a catalyst comprised of Fe₄Co₁Ni₁Mo₁Cr₂Mn₂O_{17.55-y}Sy supported on γ -Al₂O₃. The molar ratio of methane to SO₂ in the feed gas stream was 2. The catalyst (20-50 mesh) weighs 1 gr. A sulfur yield of 92.9% was obtained at 760°C. (Table 15)

2. The effect of carriers on the catalytic reduction of 66.6% SO₂ by methane at various temperatures. The catalyst (granules) were composed of Co₃O_{4-y}Sy supported on γ -Al₂O₃. The flow rates of methane and SO₂ were 1,333 ml/hr and 2,667 ml/hr, respectively. The space velocity was 5,000 h⁻¹. Based on the results of the sulfur yield, the effectiveness of the carrier followed the following order: Al₂O₃, SiO₂, molecular sieve 13X, and then molecular sieve 5A. (Table 16 a, b, c, and d)

B. Rare Earth Metal Formulations

The following test provides characteristics of inventive catalysts incorporating rare earth metals, using CO as a reductant with high SO₂ concentrations in the feed stock.

1. The reduction of 5% of SO₂ with carbon monoxide over a catalyst comprised of Pr₆O_{11-y}Sy supported on γ -Al₂O₃. The molar ratio of CO to SO₂ in the feed gas stream was 2. The catalyst (30-40 mesh) weighs 0.3 gr. A sulfur yield of 97.2% was obtained at 480°C. (Table 17)

C. Combined Transition Metal with Other Active Metal Formulations

The following test provides characteristics of inventive catalysts incorporating combined transition metal with other active metals, using methane as a reductant and high SO₂ concentrations in the feed stock.

1. The reduction of 66.6% SO₂ with methane over a catalyst comprised of Fe₂Co₁Ni₂Se₁O_{7.33-y}Sy supported on γ -Al₂O₃. The molar ratio of methane to SO₂ in the feed gas stream was 0.5. The catalyst (30-40 mesh) weighs 1 gr. A sulfur yield of 94.2% was obtained at 740°C. (Table 18)

D. Noble Metal Formulations

The following tests provide characteristics of inventive catalysts incorporating noble metals with high SO₂ concentrations in the feed stock.

1. The reduction of 33.3% SO₂ with a syngas [(H₂/CO)=3] over a catalyst comprised of Re₂O₇-ySy supported on γ-Al₂O₃. The molar ratio of syngas to SO₂ in the feed gas stream was 2, i.e. [(3H₂+CO)/SO₂]=2]. The catalyst (20-50 mesh particles) weighs 1 gr. A sulfur yield of 93.6% was obtained at 412°C. (Table 19)

2. The reduction of 66.6% SO₂ with methane over a catalyst comprised of Re₂O₇-ySy supported on γ-Al₂O₃. The molar ratio of methane to SO₂ in the feed gas stream was 2. The catalyst (20-50 mesh) weighs 1 gr. A sulfur yield of 93.6% was obtained at 780°C. (Table 20)

III. FEED GAS CONTAINING SO₂ AND GASEOUS CONTAMINANTS

SO₂ produced from industrial sources is often admixed with one or more gaseous contaminants, such as H₂O, H₂S, COS, and O₂. As reported in the literature, these contaminants drastically decrease sulfur yield when using the current catalysts.

The following tests demonstrated the superior performance of the inventive catalysts which were conducted under conditions similar to those found in Claus tail gas treatment (containing H₂O, H₂S, and COS), regenerable SO₂ scrubbers (containing H₂O and H₂S), IGCC (containing O₂), and power plant flue gas cleanup (containing O₂ and H₂O).

1. The effect of 15% of water vapor in the feed gas on the catalytic reduction of SO₂ by syngas [(H₂/CO)=3]. The catalyst (30-40 mesh) was comprised of Fe₄Co₂Ni₂Mo₁Mn₂O_{17.66}-ySy supported on alumina. The space velocity was 10,000 h⁻¹. The subscript "w" indicates runs with 15% water vapor in the feed. The results show that the sulfur yields were the same above temperatures of 440°C and that the water vapor did not affect the performance of the catalyst. (Table 21)

2. The effect of 15% water vapor in the feed gas on the catalytic reduction of SO₂ by syngas [(H₂/CO)=0.75]. The catalyst (30-40 mesh) was comprised of Fe₄Co₂Ni₂Mo₁Mn₂O_{17.66}-ySy supported on alumina. The space velocity was 10,000 h⁻¹. The subscript "w" indicates runs with 15% water vapor in the feed. The results show that sulfur yields were the same above temperatures of 440°C and that the water vapor did not effect the performance of the catalyst. (Table 22)

3. The effect of the molar ratio of syngas to SO₂ (R = [3H₂ + CO]/SO₂) on the catalytic reduction of SO₂ in the presence of 15% water vapor at 480°C. The catalyst (30-40 mesh) was comprised of Fe₄Co₂Ni₂Mo₁Mn₂O_{17.66}-ySy supported on alumina. The space velocity was

10,000 h⁻¹. A sulfur yield of 91.2% was obtained at the stoichiometric ratio, R= 2. The largest yield of sulfur (97.1%) was obtained at R=2.2. (Table 23)

4. The effect of 10% H₂S in the feed gas on the catalytic reduction of SO₂ by syngas ([H₂/CO]=3). The catalyst (30-40 mesh) was comprised of Fe₄Co₂Ni₂Mo₁Mn₂O_{17.66-y}Sy supported on alumina. The space velocity was 10,000 h⁻¹. The results show that the addition of H₂S in the feed gas did not affect the sulfur yield to any appreciable extent. (Table 24)

5. The effect of 10% COS in the feed gas on the catalytic reduction of SO₂ by syngas ([H₂/CO]=3). The catalyst (30-40 mesh) was comprised of Fe₄Co₂Ni₂Mo₁Mn₂O_{17.66-y}Sy supported on alumina. The space velocity was 10,000 h⁻¹. The results show that the addition of H₂S in the feed gas did not affect the sulfur yield in any appreciable extent. (Table 25)

6. The effect of 10% H₂S plus 10% COS in the feed gas on the catalytic reduction of SO₂ by syngas ([H₂/CO]=3). The catalyst (30-40 mesh) was comprised of Fe₄Co₂Ni₂Mo₁Mn₂O_{17.66-y}Sy supported on alumina. The space velocity was 10,000 h⁻¹. The results show that the simultaneous addition of H₂S and COS in the feed gas did not affect the sulfur yield in any appreciable extent. (Table 26)

7. The catalyst stability study in the reduction of 10% SO₂ with syngas [(H₂/CO)=1.5] containing 18% oxygen at 580°C. The catalyst was comprised of Fe₄Co₁Ni₁Mo₁Mn₂O_{15.33-y}Sy supported on γ-Al₂O₃. The molar ratio of syngas to (SO₂ + O₂) in the feed gas stream was 2. The catalyst (granules) weighs 5 gr. The catalyst shows stable catalytic activity over the entire 260 minute run. (Table 27)

8. The catalyst stability study in the reduction of 10% SO₂ with syngas [(H₂/CO)=1.5] containing 18% oxygen at 560°C. The catalyst was comprised of Fe₄Co₁Ni₁Mo₁Mn₂O_{15.33-y}Sy supported on γ-Al₂O₃. The molar ratio of syngas to (SO₂ + O₂) in the feed gas stream was 2. The catalyst (granules) weighs 5 gr. The catalyst shows a stable activity over the entire 128 minute run. (Table 28)

9. The catalyst stability study in the reduction of 10% SO₂ with syngas [(H₂/CO)=1.5] containing 18% oxygen at 540°C. The catalyst was comprised of Fe₄Co₁Ni₁Mo₁Mn₂O_{15.33-y}Sy supported on γ-Al₂O₃. The molar ratio of syngas to (SO₂ + O₂) in the feed gas stream was 2. The catalyst (granules) weighs 5 gr. The catalyst shows a stable activity over the entire run of 76 minutes. (Table 29)

Example 1 SULFIDATION BY GAS REACTION Fe₄Co₂Ni₂Mn₂Mo₁O_{17.67-x}S_x/γ-Al₂O₃

1. The following metal nitrates were dissolved in 100 ml H₂O;

Fe(NO ₃) ₃ 9H ₂ O	42.6538 g	F.W. 404	Acros Organics NJ
Co(NO ₃) ₃ 6H ₂ O	15.3633 g	F.W. 291.03	Aldrich Chem.
Ni(NO ₃) ₂ 6H ₂ O	15.3517 g	F.W. 290.81	Aldrich Chem.
Mn(NO ₃) ₂ 6H ₂ O	15.4598 g	F.W. 287.04	Aldrich Chem.

2. 100g of γ -alumina (γ -Al₂O₃) were added to the nitrate solution in a vessel. The γ -aluminum oxide substrate [γ -Al₂O₃] was obtained from A. Johnson Matthey Company, Word Hill, MA, FW 1001.96; 96+% including 3% C. They were in the form of approximately 3.2 mm tablets with a surface area of 175m²/g and a density of 3.5-3.9.

The mixture was then stirred in a crucible placed on a heating pad until the mixture was dry. This step removed water and decomposed the nitrates.

3. The solid mixture of step 2 was heated in a Muffle oven at 200°C for 0.5 hour and then at 450°C for 1 hour to further decompose the nitrate components. The Muffle oven was then turned off and allowed to equilibrate to room temperature. The solid mixtures were then removed.

4. 4.6601 g of (NH₄)₆Mo₇O₂₄·4H₂O (F.W. 1235.86 from Aldrich Chemical) was dissolved in 100 ml of a 10% aqueous ammonium hydroxide solution, i.e. containing 10 ml of NH₄OH.

5. The solutions produced in step 4 were then added to the solids mixtures produced in step 3. This mixtures was then gently stirred while heating in a crucible on a heating pad set for 200°C, to dryness and to remove ammonia.

6. The solid mixture produced in step 5 were then calcined in a Muffle oven in a stepwise manner at 250°C for 0.5 hours, 450°C for 0.5 hours, and 600°C for 4 hours. The oven was then switched off and allowed to equilibrate to ambient temperature. The solid mixture was then removed.

7. The solid mixture of step 6 was sulfided with 20-30% H₂S (the balance N₂) at a space velocity of 1,000 ml/gh at 600°C. The sulfidation is completed when the outlet H₂S concentration reaches the inlet H₂S concentration

Example 2 SULFIDATION BY SOLUTION Fe₄Co₂Ni₂Mn₂Mo₁S_{17.67}/γ-Al₂O₃

1&2. In these steps, metal nitrates in solution were used to impregnate an alumina substrate as described in Example 1.

3. 172.2 mol of 20% $(\text{NH}_4)_2\text{S}$ solution at 30% excess, (F.W. 68.06, 20-24% in water from Johnson Matthey) was added to a solid mixture made in steps 1 and 2. The resulting solution was heated to dryness in a crucible placed on a heating pad set to 100°C.
4. 4.6601 g of $(\text{NH}_4)_6\text{Mo}_7\text{O}_{24} \cdot 4\text{H}_2\text{O}$ was dissolved in 100 ml of a 10% aqueous ammonium hydroxide solution, that is containing 10 ml of NH_4OH and 90 ml water.
5. The solid mixtures of step 3 were then added into the solution of step 4. This mixtures was gently stirred in a crucible placed on a heating pad at 100°C until it was dry.
6. The solid mixture produced in step 5 was added to a solution of 35 ml aqueous $(\text{NH}_4)_2\text{S}$ (20% concentration) and 65 ml of water. Then, the solution was heated to dryness in a crucible placed on a heating pad set to 100°C.
7. The solid mixtures produced in step 6 were activated in a quartz reactor under nitrogen gas in a stepwise manner at 250°C for 0.5 hours, 450°C for 0.5 hours and 600°C for 4 hours. The power for heating the quartz reactor was then turned off, and the temperature allowed to equilibrate to ambient temperatures. The final catalyst was then removed.

CLAIMS:

1. A sulfide catalyst for the conversion of sulfur dioxide to elemental sulfur comprising;
 - A. Fe, Co or Ni sulfides, either singly or in combination,
 - B. Mo, Mn, Cu, W, V or Cr sulfides, either singly or in combination, and
 - C. a carrier,
 the composition of said catalyst being represented by the formula:

$$\text{Fe}_a\text{Co}_b\text{Ni}_c\text{Cr}_d\text{Mn}_e\text{Mo}_f\text{V}_g\text{Cu}_h\text{W}_i\text{O}_x\text{S}_y$$
 wherein a, b, c, d, e and f are independently ranged between 0 and 30, g and h are between 0 and 10, i is between 0 and 5, and x+y is determined by the charge balance of the catalyst, and the proportion of x:y at the active surface of the catalyst is between about 0:1 and 1:0.1.
2. The catalyst of Claim 1, wherein the proportion of x:y is in the range of about 0:1 to 1:0.5.
3. The catalyst of Claim 2, wherein the proportion of x:y is in the range of about 0:1 to 1:1.
4. The catalyst of Claim 1, wherein the formulation of the catalyst is selected from $\text{Fe}_4\text{Co}_2\text{Ni}_2\text{Mo}_1\text{Mn}_4\text{O}_{17.66-y}\text{S}_y$, $\text{Fe}_4\text{Co}_1\text{Ni}_1\text{Mo}_1\text{Mn}_4\text{O}_{15.33-y}\text{S}_y$, $\text{Fe}_4\text{Co}_1\text{Ni}_1\text{Mo}_1\text{Cr}_2\text{Mn}_2\text{O}_{17.55-y}\text{S}_y$, $\text{Fe}_4\text{Co}_2\text{Ni}_2\text{Mo}_1\text{Mn}_2\text{S}_{17.66}$, $\text{Fe}_4\text{Co}_1\text{Ni}_1\text{Mn}_1\text{Cu}_2\text{V}_8\text{O}_{32.33-y}\text{S}_y$
5. The catalyst of Claim 1, additionally comprising a rare earth metal sulfide.
6. The catalyst of Claim 5, wherein the rare earth metal sulfide comprises La, Ce, Pr, and Nd.
7. The catalyst of Claim 6, wherein the formulation of the catalyst is $\text{Fe}_4\text{Co}_1\text{Ni}_1\text{Mo}_1\text{Pr}_6\text{Mn}_2\text{O}_{26.33-y}\text{S}_y$, $\text{Fe}_4\text{Co}_1\text{Ni}_1\text{Mo}_1\text{La}_6\text{Mn}_2\text{O}_{26.33-y}\text{S}_y$,

$\text{Fe}_4\text{Co}_1\text{Ni}_1\text{Mo}_1\text{Ce}_6\text{Mn}_2\text{O}_{26.33-y}\text{S}_y$,
 $\text{Fe}_4\text{Co}_1\text{Ni}_1\text{Mn}_1\text{Cu}_5\text{Pr}_5\text{O}_{24.5-y}\text{S}_y$.

$\text{Fe}_4\text{Co}_1\text{Ni}_1\text{Mo}_1\text{Nd}_6\text{Mn}_2\text{O}_{26.33-y}\text{S}_y$,

and

8. The catalyst of Claim 1, additionally comprising an active metal sulfide.

9. The catalyst of Claim 8, wherein said active metal sulfide is selected from Zn, Mg, Ca, Se, Bi, Li, Na, K, and Cs.

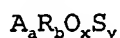
10. The catalyst of Claim 9, wherein the formulation of the catalyst is selected from $\text{Fe}_1\text{Co}_1\text{Ni}_1\text{Bi}_5\text{Cu}_5\text{O}_{16.33-y}\text{S}_y$,
 $\text{Fe}_1\text{Co}_1\text{Ni}_1\text{Zn}_5\text{Cu}_5\text{O}_{16.33-y}\text{S}_y$, $\text{Fe}_1\text{Co}_1\text{Ni}_1\text{Mg}_5\text{Cu}_5\text{O}_{16.33-y}\text{S}_y$, $\text{Fe}_1\text{Co}_1\text{Ni}_1\text{Ca}_5\text{Cu}_5\text{O}_{16.33-y}\text{S}_y$,
 $\text{Fe}_1\text{Co}_1\text{Ni}_1\text{Se}_5\text{Cu}_5\text{O}_{16.33-y}\text{S}_y$, $\text{Fe}_2\text{Mg}_1\text{Li}_1\text{Pr}_2\text{Cu}_2\text{Bi}_2\text{O}_{12.67-y}\text{S}_y$,
 $\text{Fe}_4\text{Co}_1\text{Ni}_1\text{Mn}_1\text{Cu}_2\text{Li}_8\text{O}_{15.33-y}\text{S}_y$, $\text{Fe}_2\text{Mg}_1\text{Na}_1\text{Pr}_2\text{Cu}_2\text{Bi}_2\text{O}_{12.67-y}\text{S}_y$, and
 $\text{Fe}_4\text{Co}_1\text{Ni}_1\text{Mn}_1\text{Cu}_2\text{Na}_8\text{O}_{15.33-y}\text{S}_y$,

11. A sulfide catalyst for the conversion of sulfur dioxide to elemental sulfur which has a high conversion rate in the presence of low levels or in the absence of H_2O and H_2 , comprising;

A. a component selected from Li, Na, K, Cs, La, Ce, Pr, sulfides, or mixtures thereof, and

B. a carrier,

the composition of said catalyst being represented by the formula:



where A is an alkali metal,

R is a rare earth metal,

a and b are independently ranged between 0 and 30,

x+y is determined by the charge balance of the catalyst, and

the proportion of x:y is between about 0:1 and 1:0.1.

12. The catalyst of Claim 11, wherein the formulation is selected from $\text{Li}_2\text{O}_{1-y}\text{S}_y$, $\text{Na}_2\text{O}_{1-y}\text{S}_y$, $\text{K}_2\text{O}_{1-y}\text{S}_y$, $\text{Cs}_2\text{O}_{1-y}\text{S}_y$, $\text{Pr}_6\text{O}_{11-y}\text{S}_y$, $\text{Ce}_6\text{O}_{11-y}\text{S}_y$, $\text{La}_6\text{O}_{11-y}\text{S}_y$,

13. A method of producing the catalyst of Claim 1 using sulfiding gas, comprising;

a) impregnating an alumina substrate with a solution of the metal nitratesalts reflecting the desired formulation,

b) drying said impregnated alumina substrate,

- c) removing crystalline water from the dry impregnated alumina substrate,
- d) decomposing the nitrate components of the impregnated alumina substrate
- e) calcinating the impregnated substrate
- f) gaseous sulfiding the impregnated, calcinated substrate.

14. The method of Claim 13, wherein in step a), the alumina substrate is select from alpha alumina, beta alumina, or gama alumina.

15. The method of Claim 13, wherein in step b), the solution is evaporated by vacuum, gentle heating, or allowing the solution to evaporate at ambient temperatures.

16. The method of Claim 13, wherein in step b), the solution is evaporated by heating to a temperature under about 200°C.

17. The method of Claim 16, wherein the solution is evaporated by heating to a temperature between about 100°C to 150°C.

18. The method of Claim 13, wherein in step c), the crystalline water removal temperature is from 200°C to 300°C.

19. The method of Claim 18, wherein the temperature is about 250c.

20. The method of Claim 13, wherein in step d), the impregnated substrate is heated to between 300°C and 450°C.

21. The method of Claim 20, wherein the substrate is heated to about 400°C.

22. The method of Claim 13, step d), wherein the substrate is heated for about 15 minutes to 6 hours.

23. The method of Claim 13, step e), wherein the calcination temperatures is from 500°C to 700°C.

24. The method of Claim 23, wherein the calcination is at about 600°C.
25. The method of Claim 23, wherein the calcination occurs from about 2 hours to 2 days.
26. The method of Claim 25, wherein the calcination occurs for about 4 hours.
27. The method of Claim 13, wherein in step f), the sulfidation temperature is from about 200°C to 700°C.
28. The method of Claim 27, wherein the sulfidation temperature is from about 350°C to 650°C.
29. The method of Claim 28, wherein the sulfidation temperature is from about 500°C to 620°C.
30. The method of Claim 13, wherein in step f) the sulfidation time is from about 10 minutes to five days.
31. The method of Claim 30, wherein the sulfidation time is from about 30 minutes to 24 hours.
32. The method of Claim 31, wherein the sulfidation time is about an hours.
33. The method of Claim 13, in step f) wherein the sulfiding gas concentration is from about 0.1% to 100%.
34. The method of Claim 33, wherein the concentration is from about 5%-40%.
35. The method of Claim 34, wherein the concentration is about 10%.

36. The method of Claim 13, wherein in step f) the gases used to treat the substrate are selected from the group of hydrogen sulfide gas, sulfur dioxide in a methane stream [SO_2/CH_4], sulfur dioxide in a hydrogen stream [SO_2/H_2], and sulfur dioxide in a carbon monoxide stream [SO_2/CO] or combinations thereof.

37. A method of producing the catalyst of Claim 1 using a sulfiding liquid comprising;

- a) impregnating an alumina substrate with a solution of the metal salts reflecting the desired formulation,
- b) drying said impregnated alumina substrate,
- c) treating the impregnated alumina substrate with a sulfiding solution,
- d) drying said sulfiding solution treated impregnated substrate,
- e) removing crystalline water from the dry impregnated alumina substrate,
- f) decomposing the nitrate components of the impregnated alumina substrate
- g) calcinating the impregnated substrate

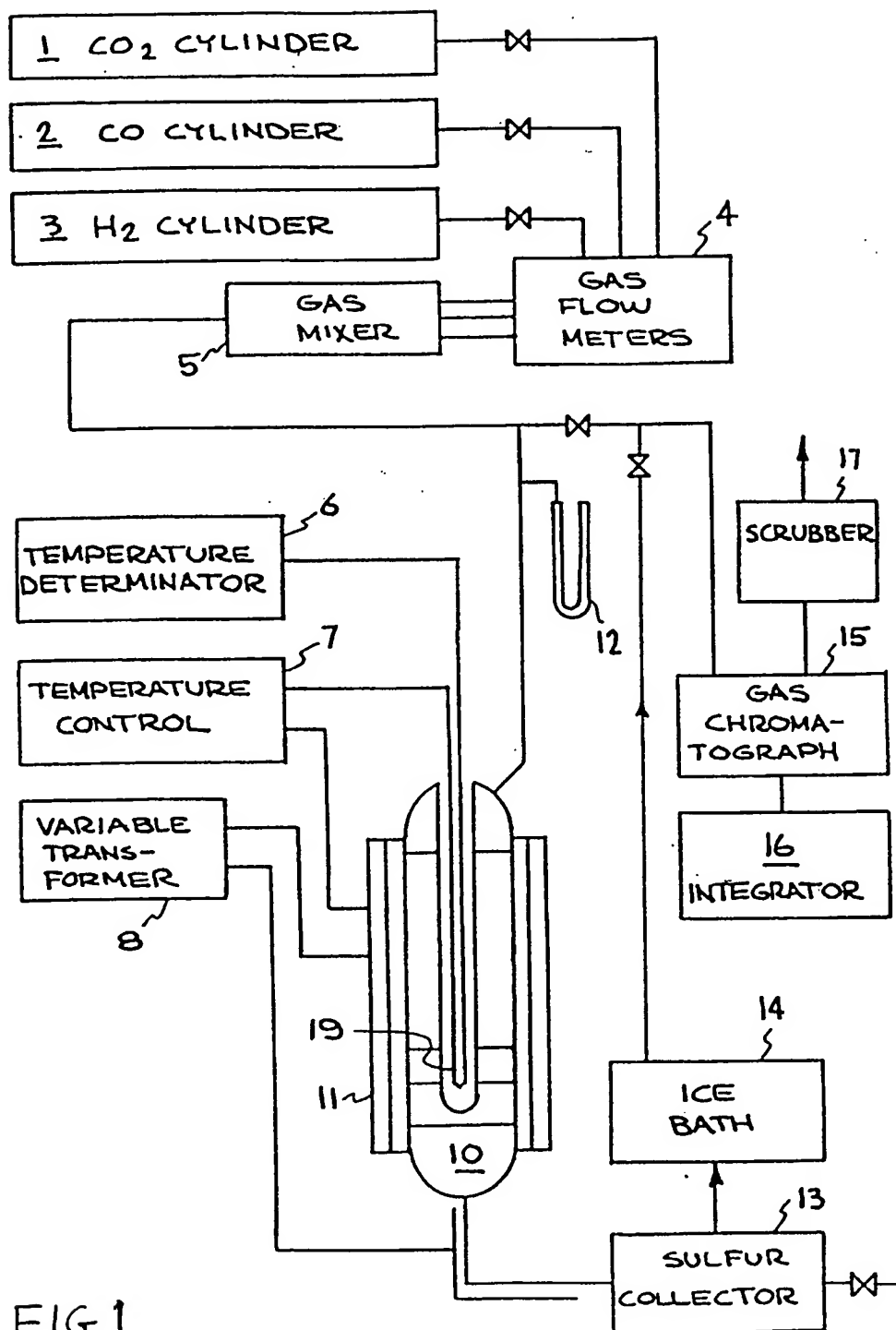
38. The method of Claim 37, wherein in step a), the alumina substrate is select from alpha alumina, beta alumina, or gama alumina.

39. The method of Claim 37, wherein in step b), the solution is evaporated by vacuum, gentle heating, or allowing the solution to evaporate at ambient temperatures.

40. The method of Claim 37, wherein in step b) and d), the solution is evaporated by heating to a temperature under about 200°C.

41. The method of Claim 40, wherein the solution is evaporated by heating to a temperature between about 100°C to 150°C.

42. The method of Claim 37, wherein in step c), the sulfiding solutions is provided in stoichiometric proportions to the metallic components, with an excess of sulfiding solution.
43. The method of Claim 42, wherein the excess is about 10%.
44. The method of Claim 13, wherein in step c) the sulfiding solution ranges from about 5% to 30% concentration.
45. The method of Claim 44, wherein the sulfiding solution is about a 10% concentration.
46. The method of Claim 37, wherein in step e), the crystalline water removal temperature is from 200°C to 300°C.
47. The method of Claim 46, wherein the temperature is about 250°C.
48. The method of Claim 37, wherein in step f), the impregnated substrate is heated to between about 300°C and 450°C.
49. The method of Claim 48, wherein the substrate is heated to about 400°C.
50. The method of Claim 37, step f), wherein the substrate is heated for about 15 minutes to 6 hours.
51. The method of Claim 37, step g), wherein the calcination temperatures is from 500°C to 700°C.
52. The method of Claim 51, wherein the calcination is at about 600°C.
53. The method of Claim 37, wherein in step g) the calcination occurs from about 2 hours to 2 days.
54. The method of Claim 53, wherein the calcination occurs for about 4 hours.



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TABLE 1

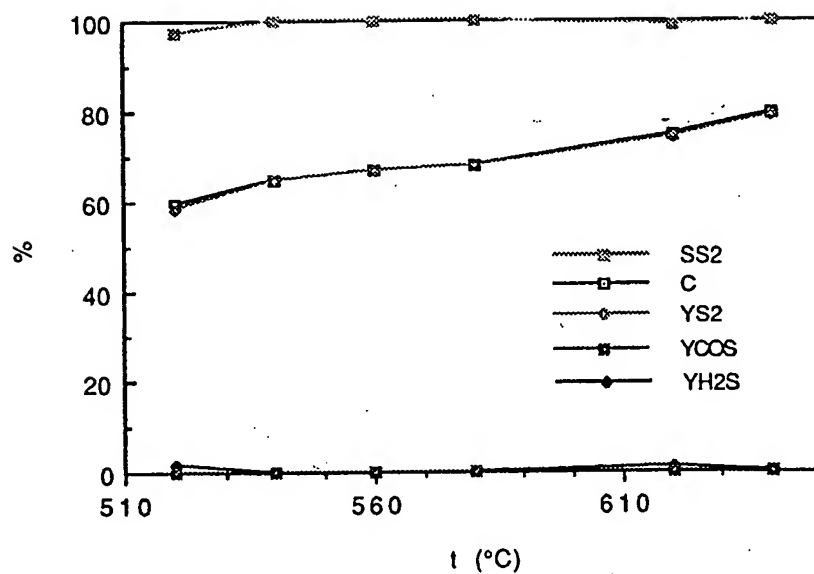


TABLE 2

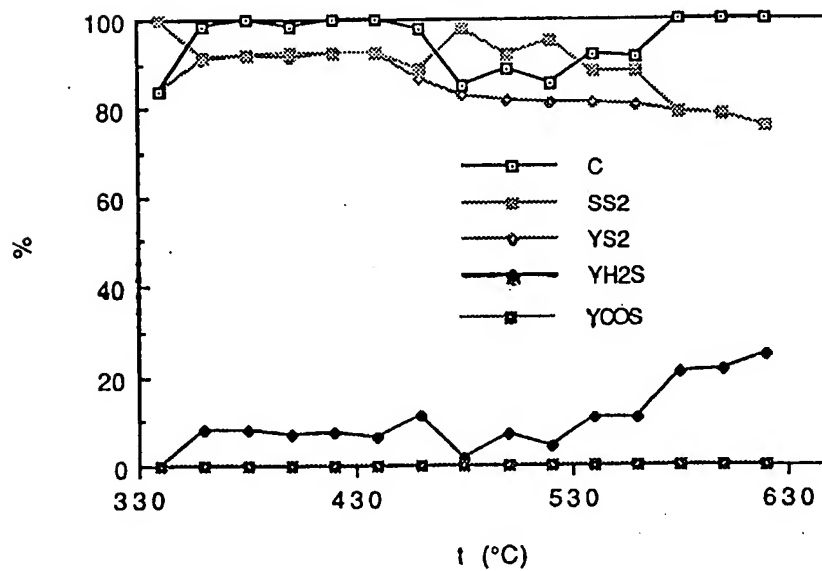


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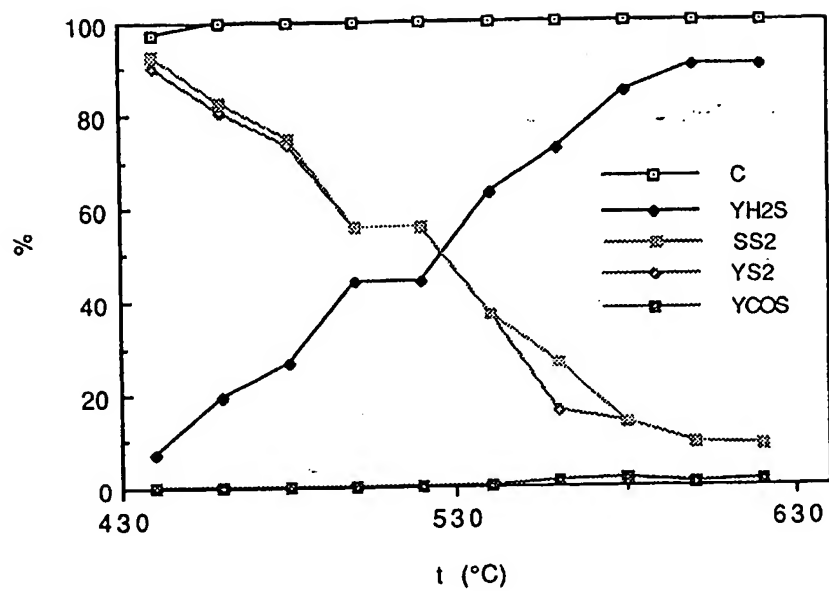


TABLE 4a

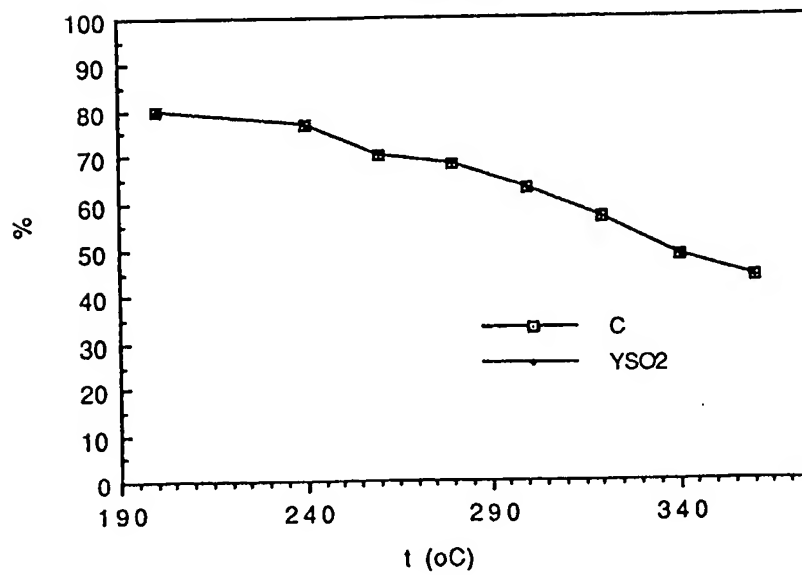


TABLE 4b

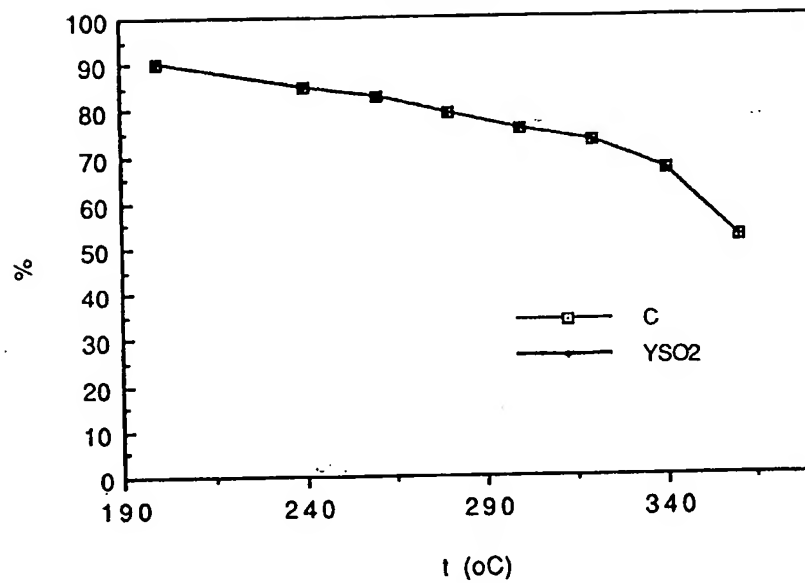


TABLE 4c

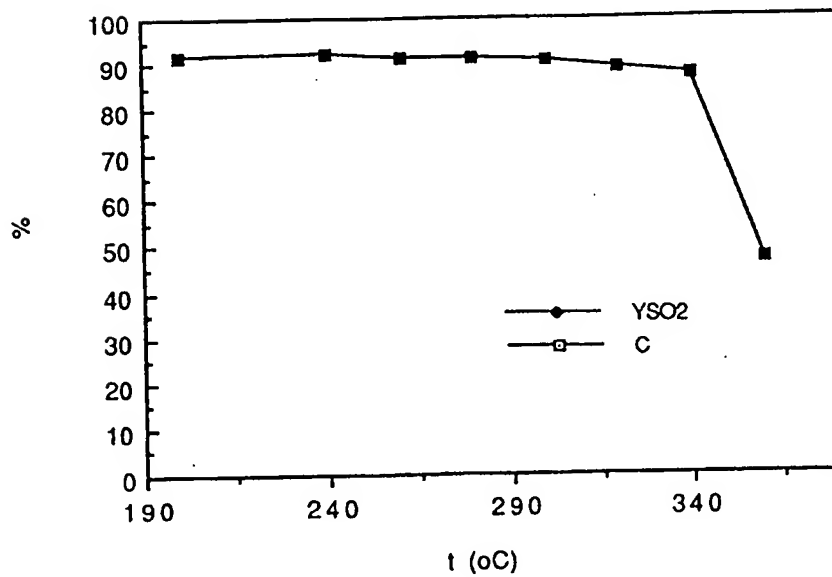


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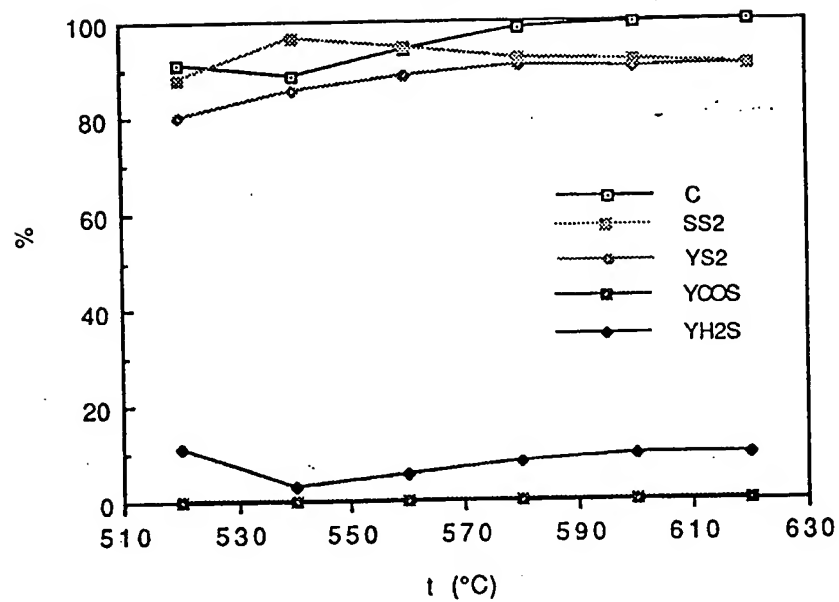
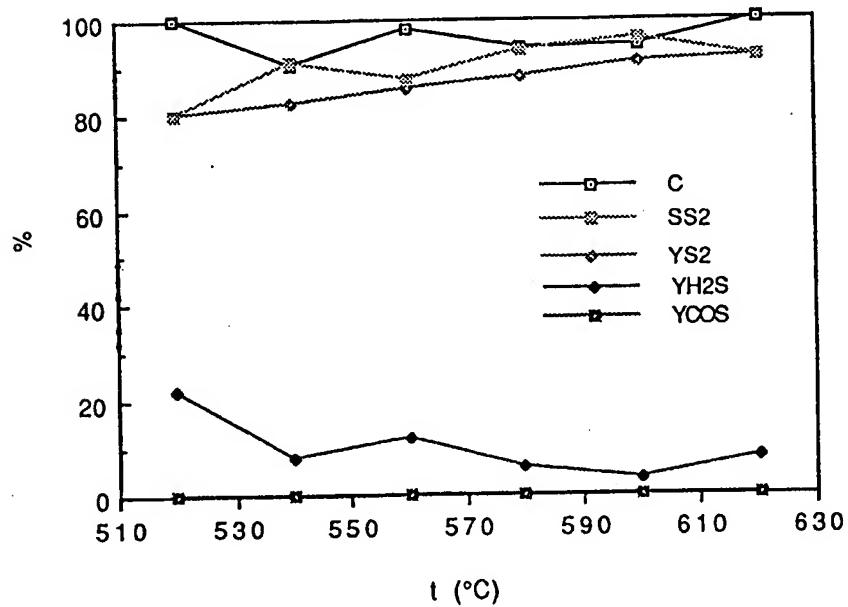


TABLE 6



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TABLE 7

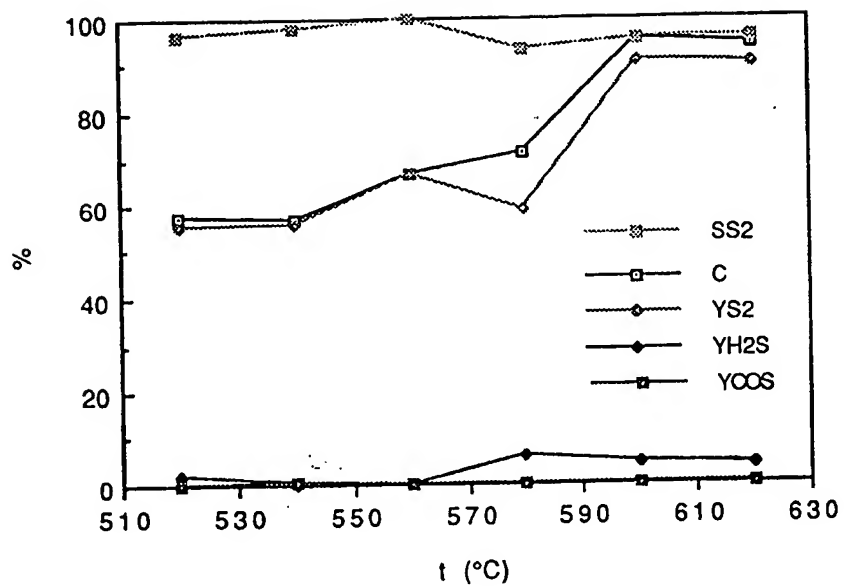
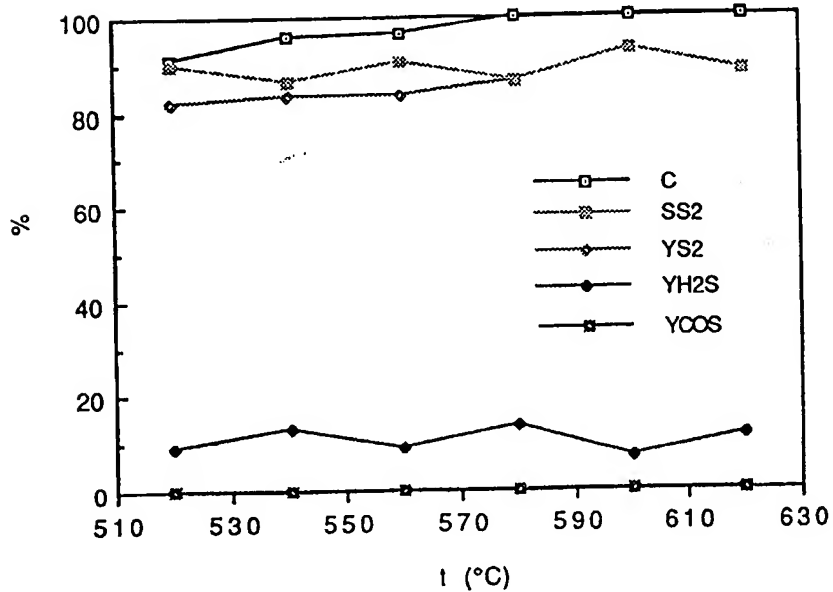


TABLE 8



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TABLE 9

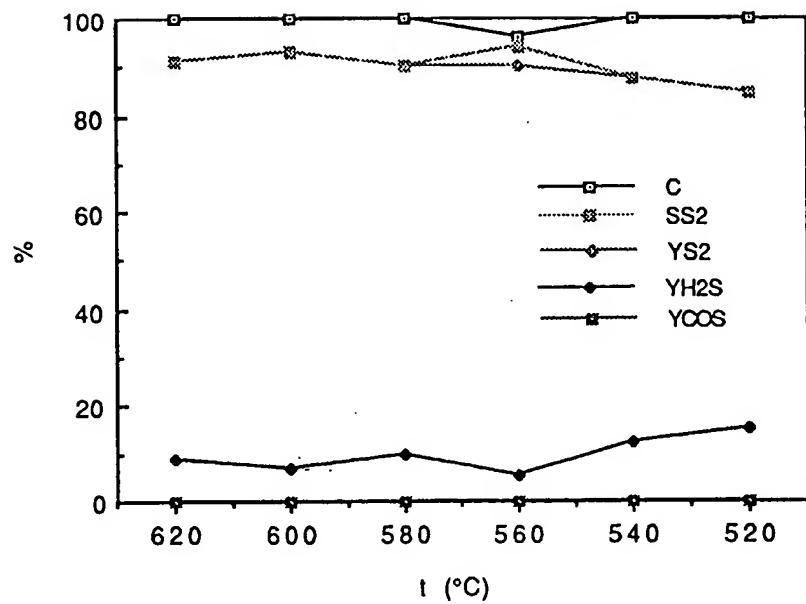


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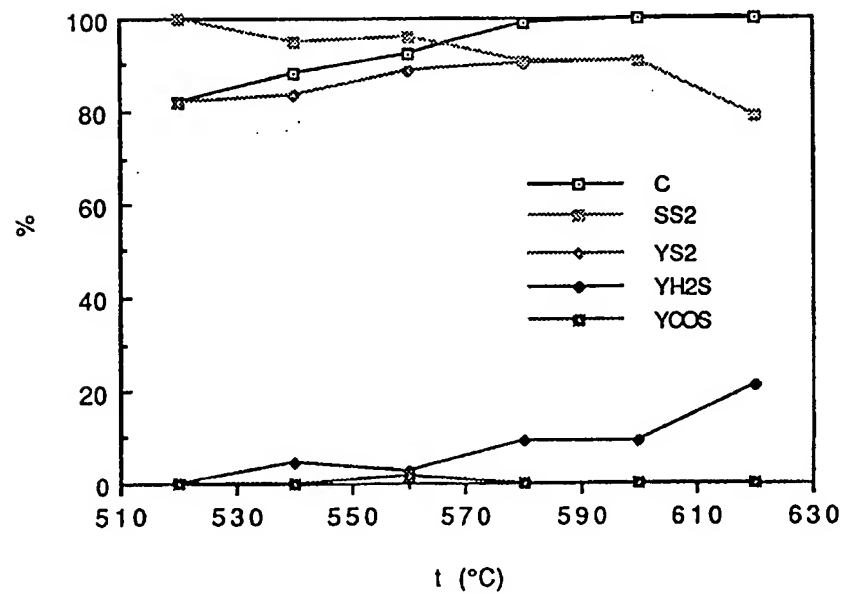


TABLE 11

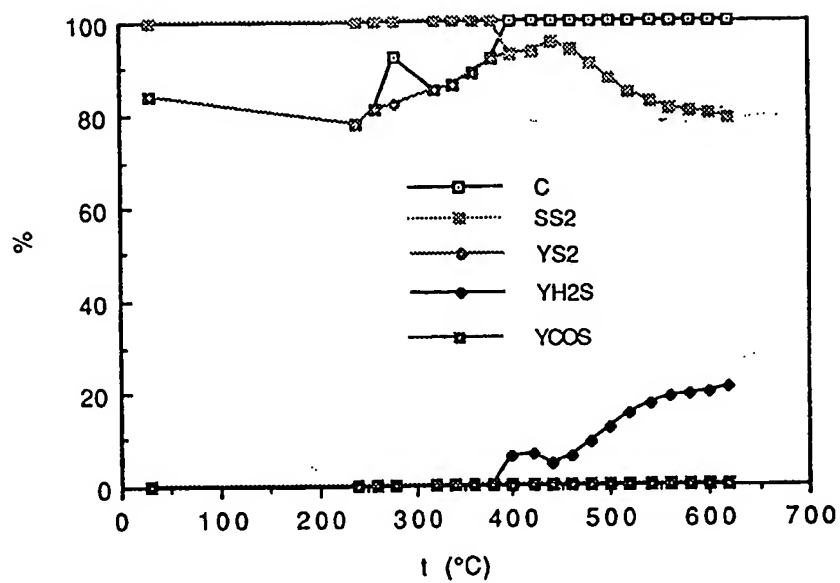


TABLE 12

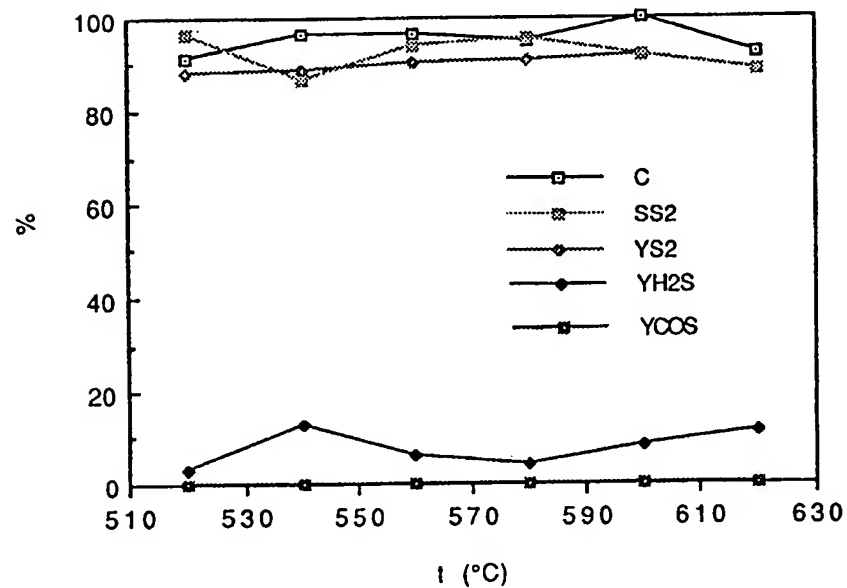


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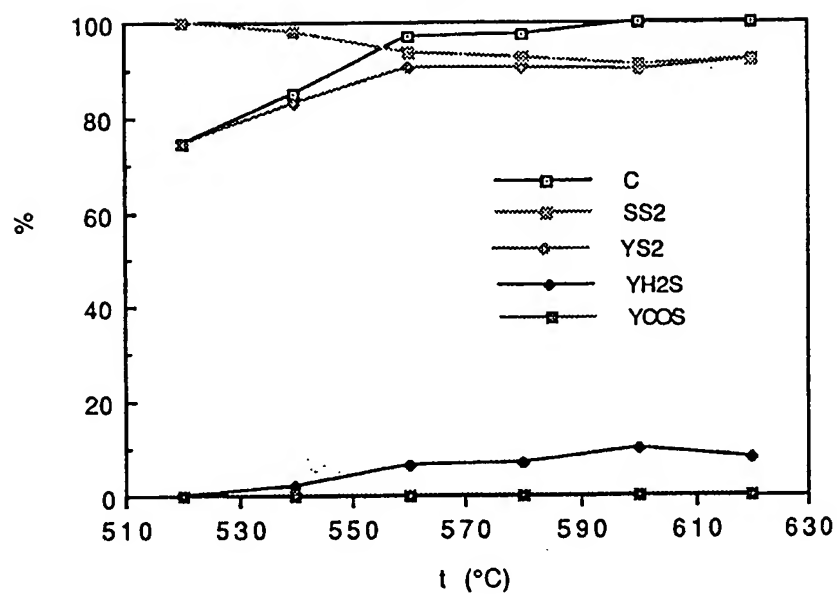
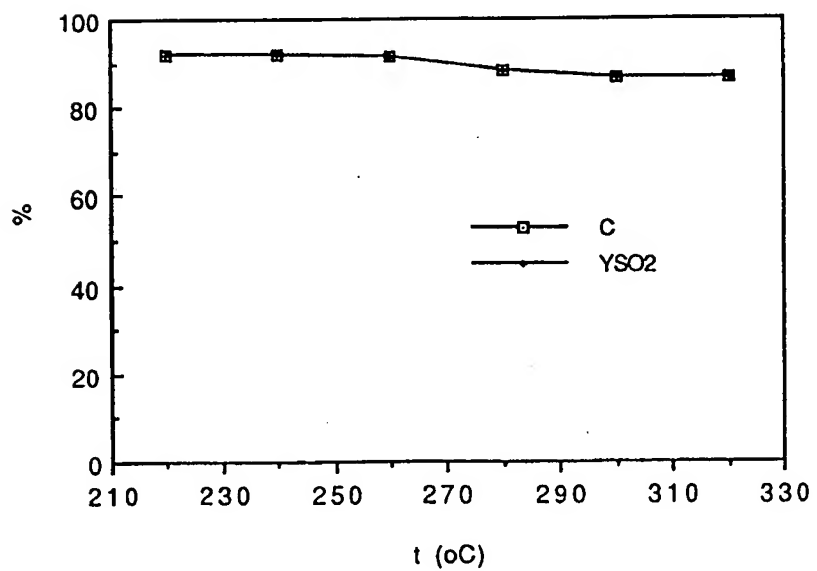


TABLE 14a



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TABLE 14b

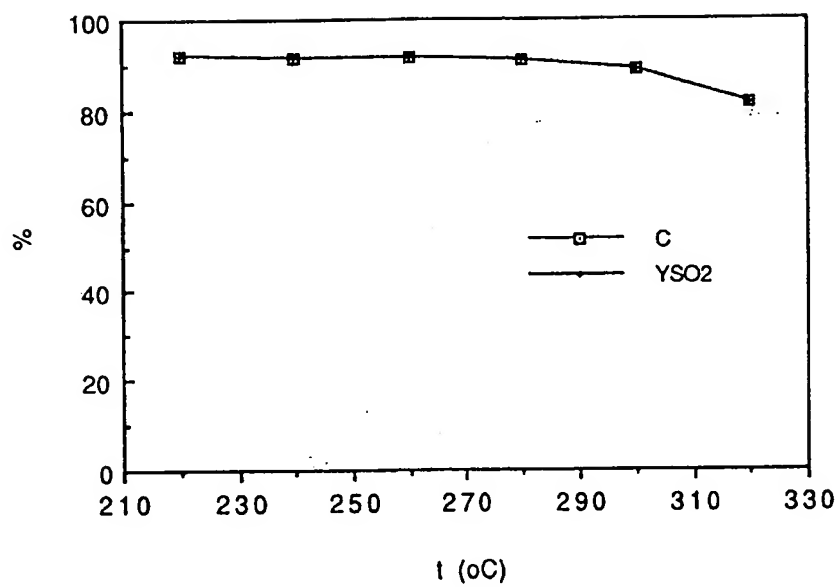


TABLE 14c

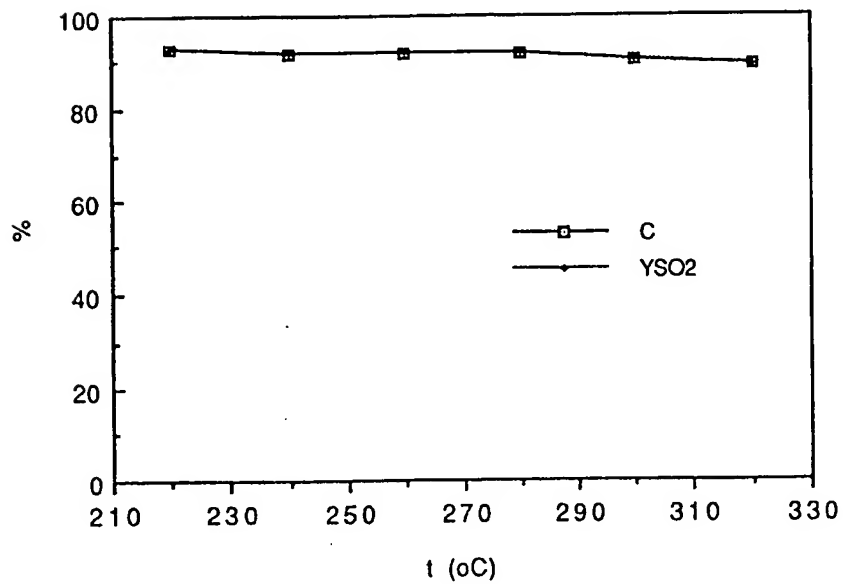


TABLE 15

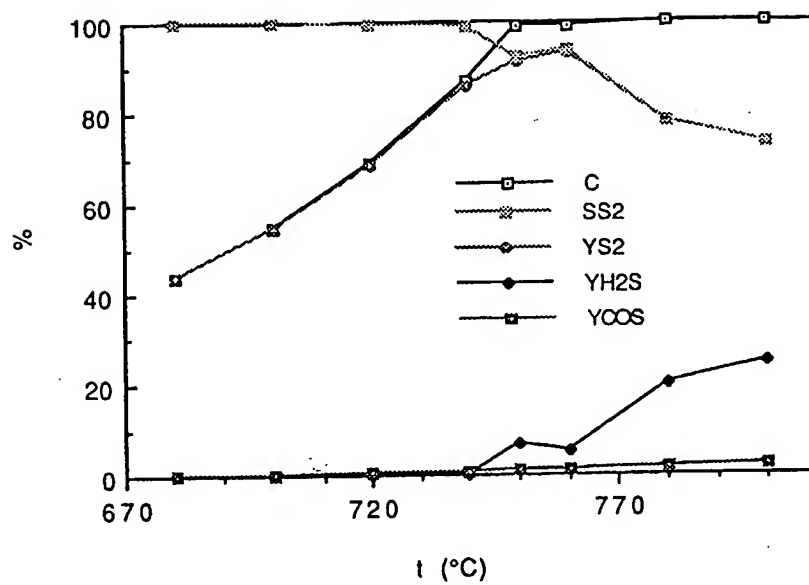


TABLE 16a

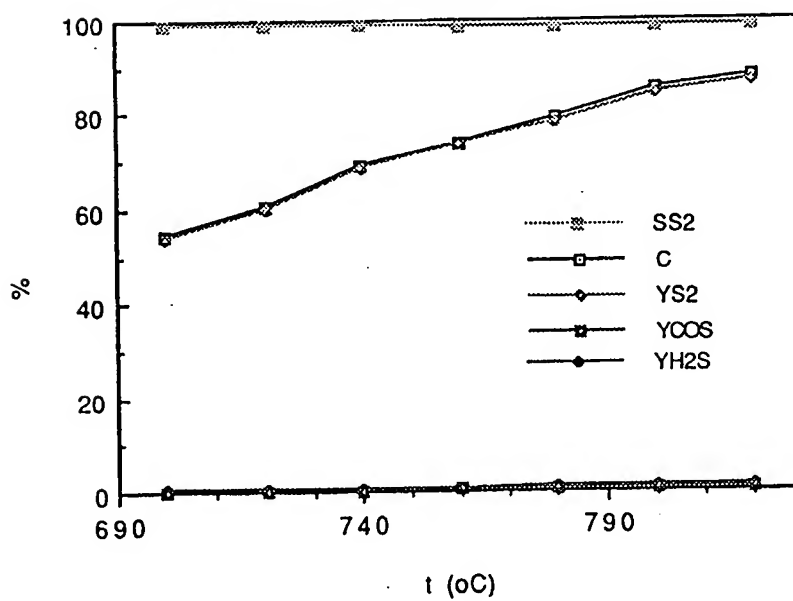


TABLE 16b

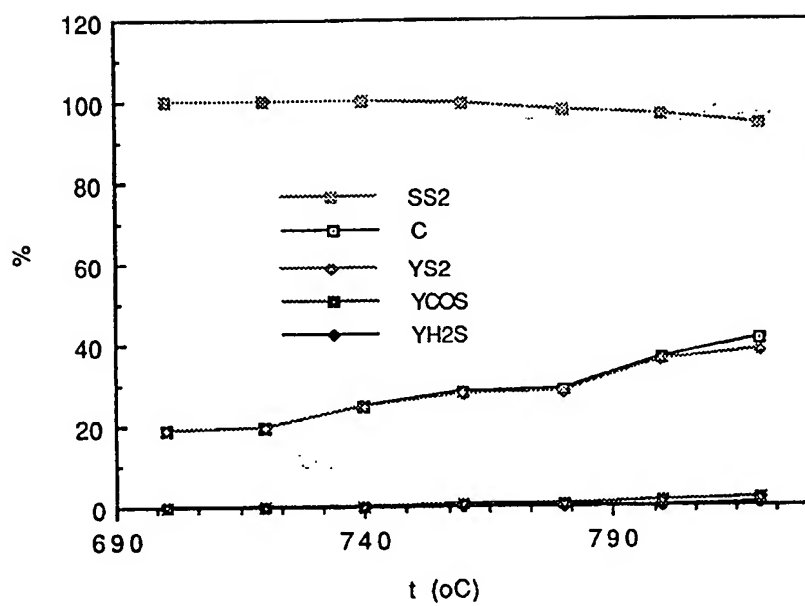
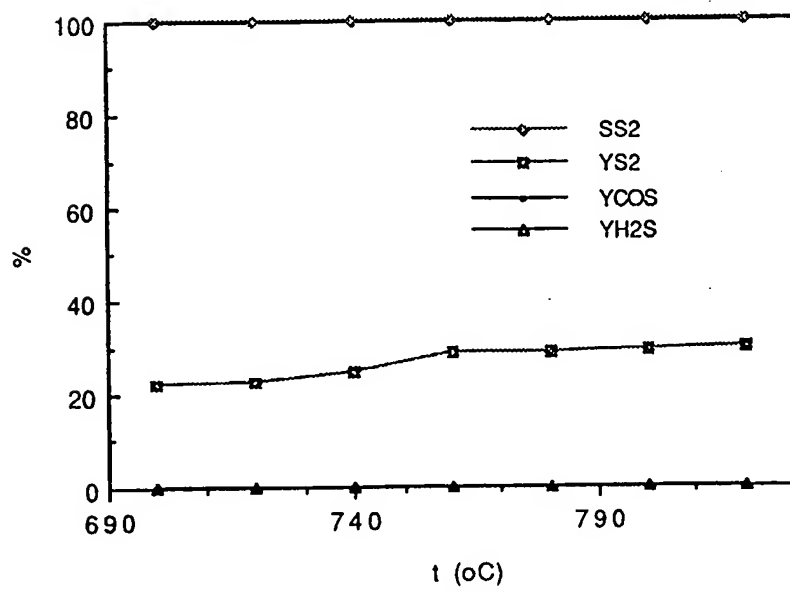


TABLE 16c



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TABLE 16d

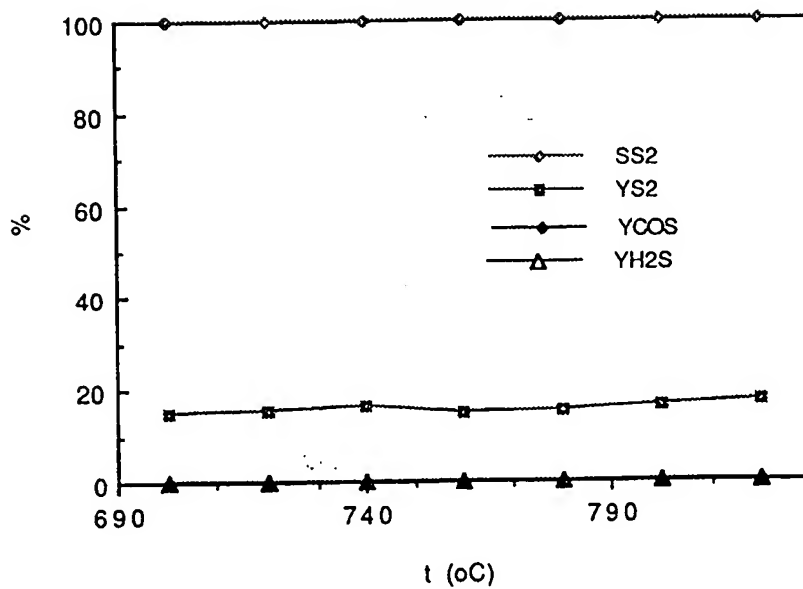
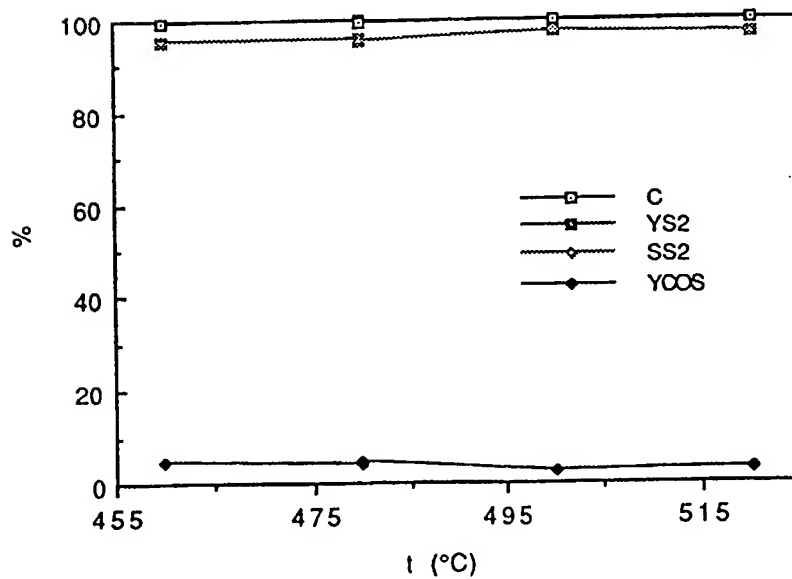


TABLE 17



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TABLE 18

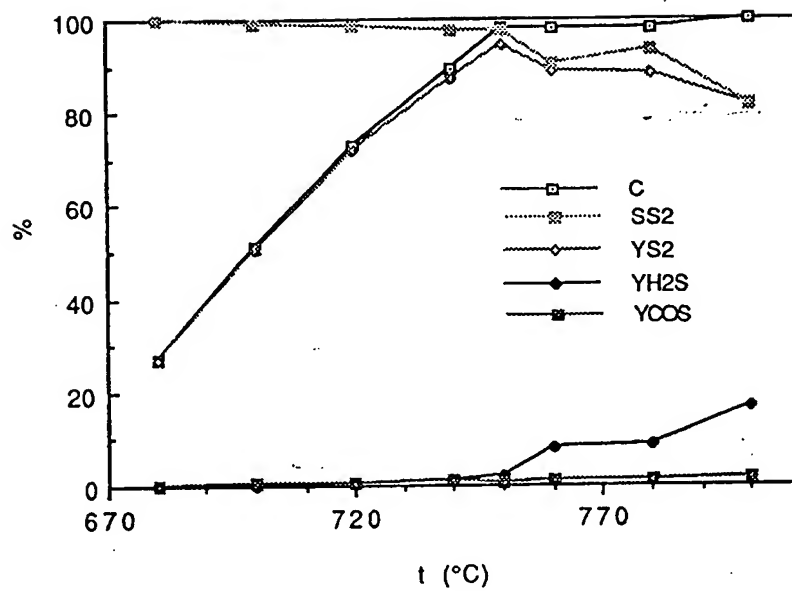
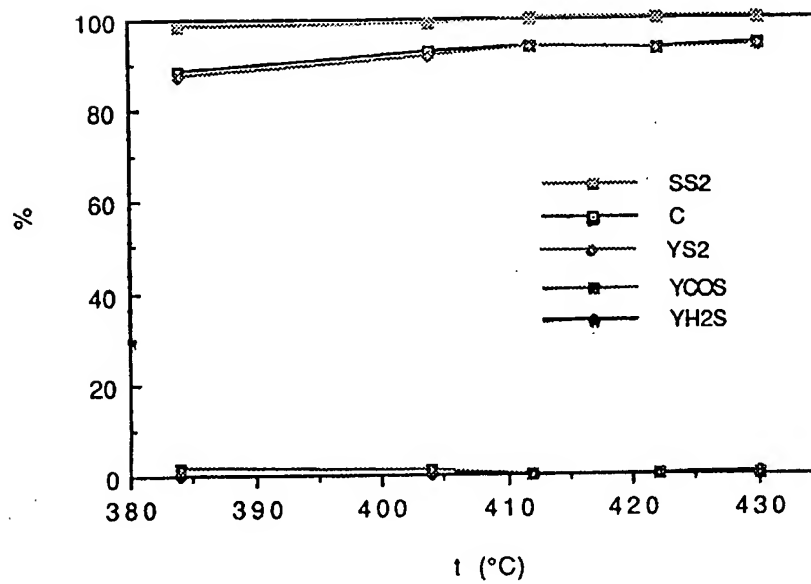


TABLE 19



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TABLE 20

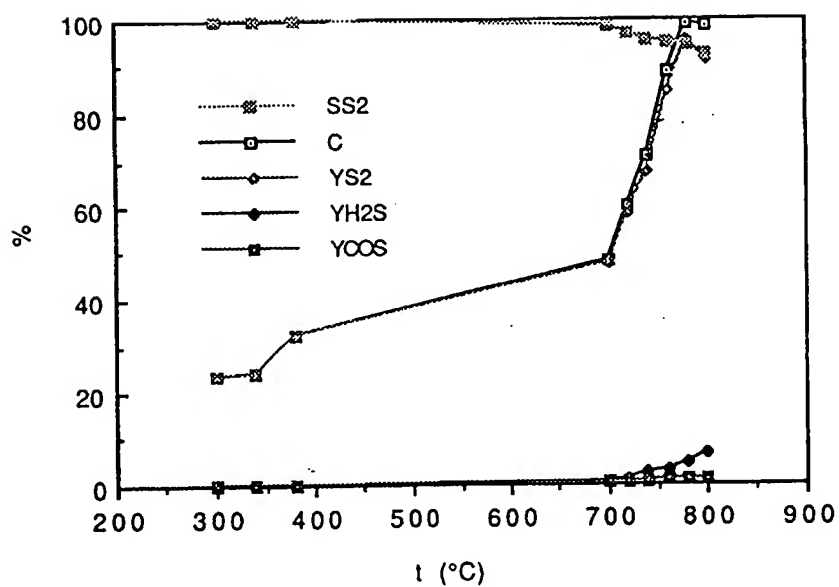
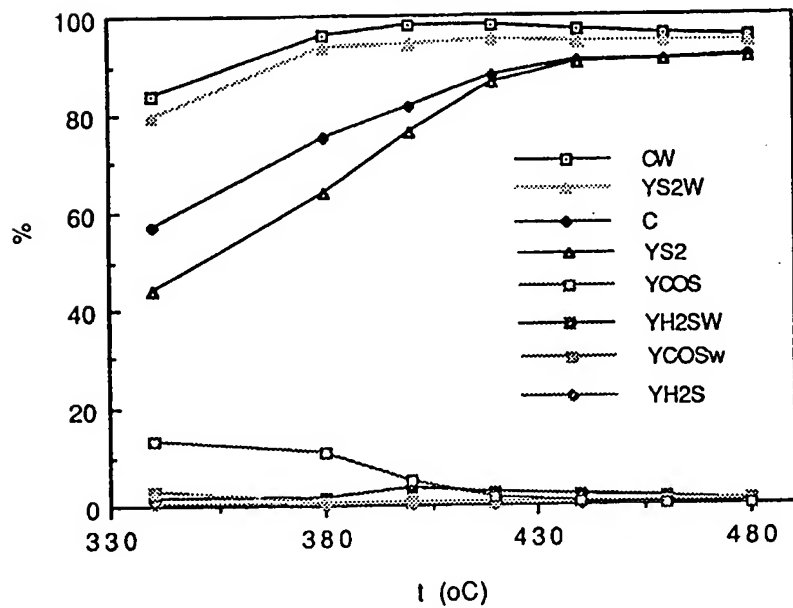


TABLE 21



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TABLE 22

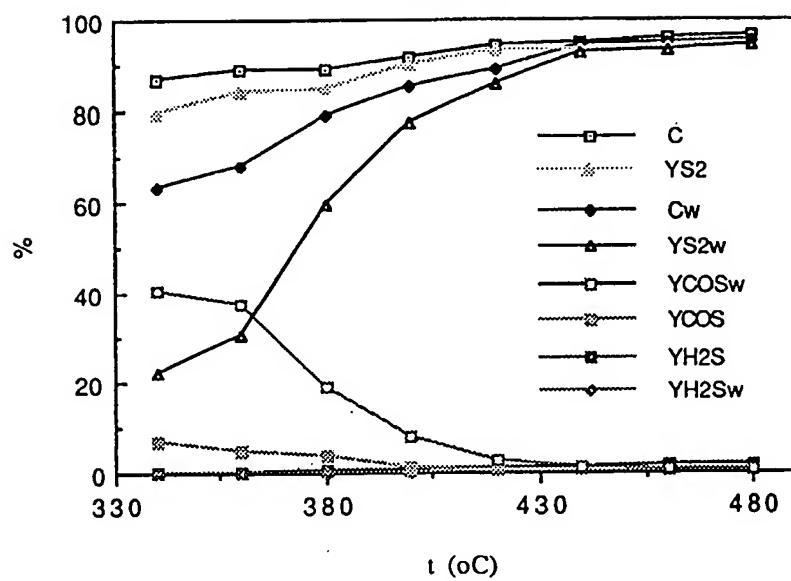


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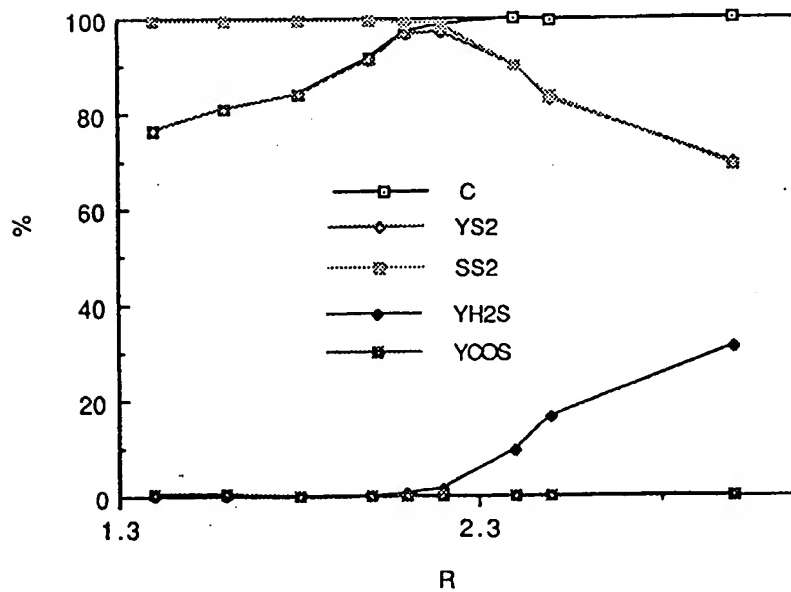


TABLE 24

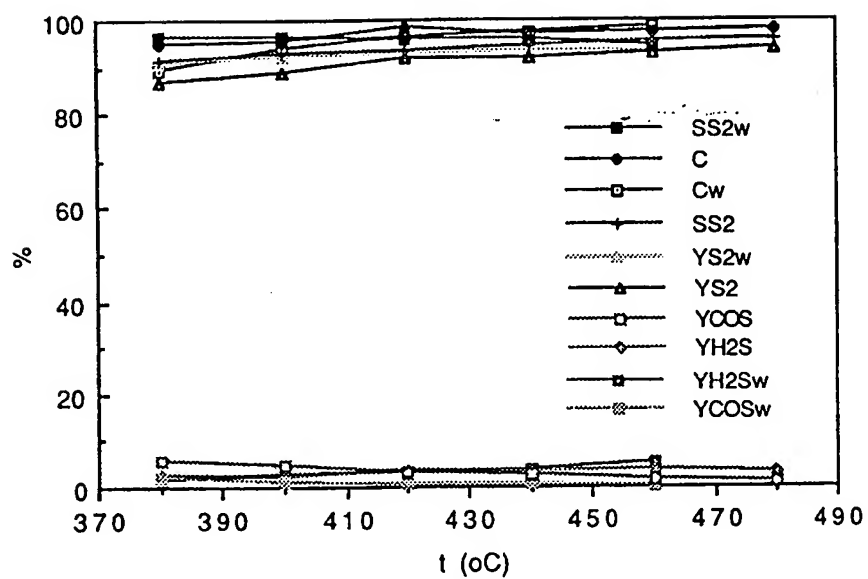


TABLE 25

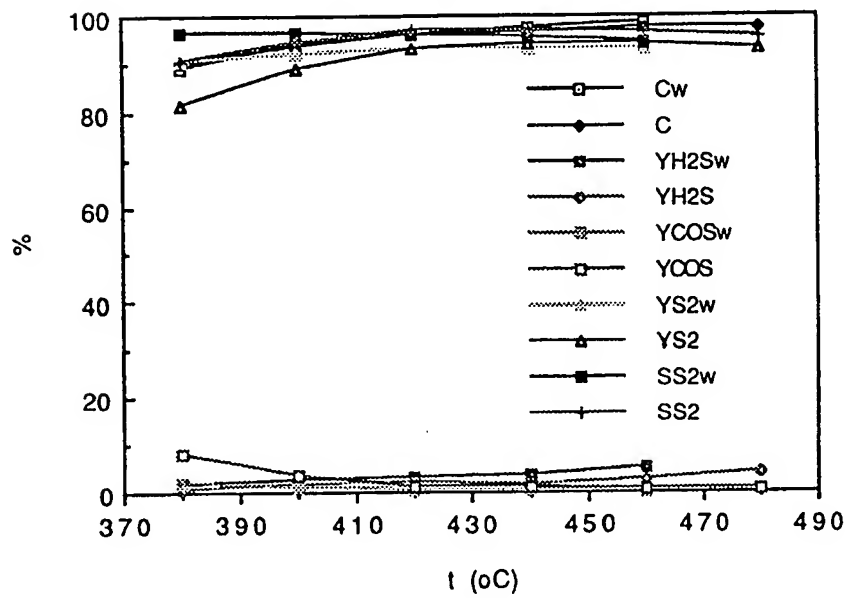


TABLE 26

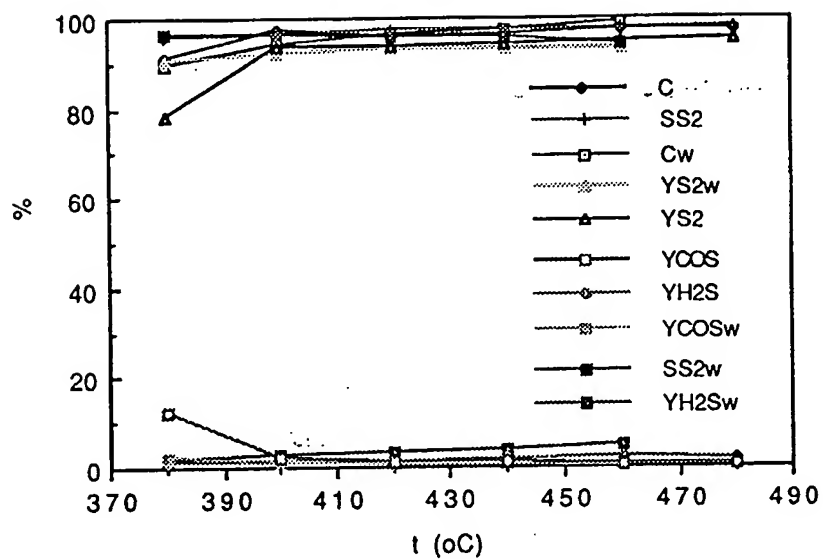


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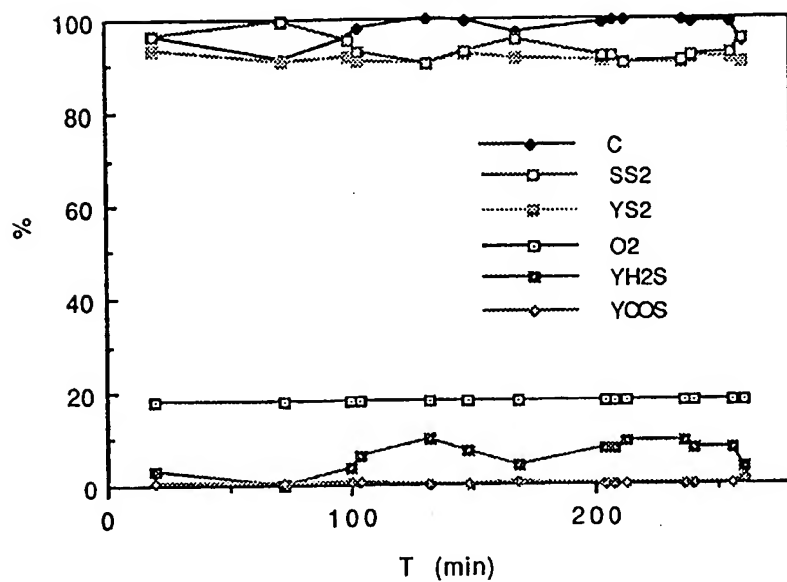


TABLE 28

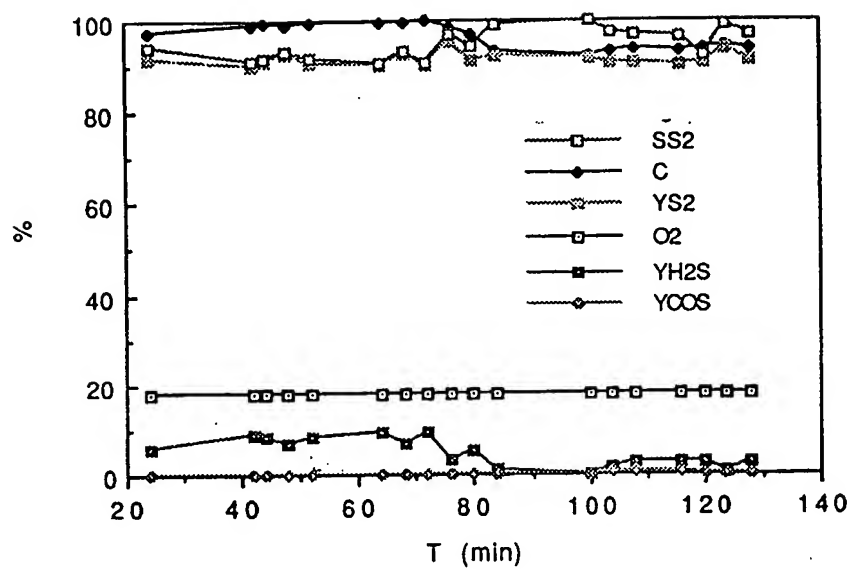
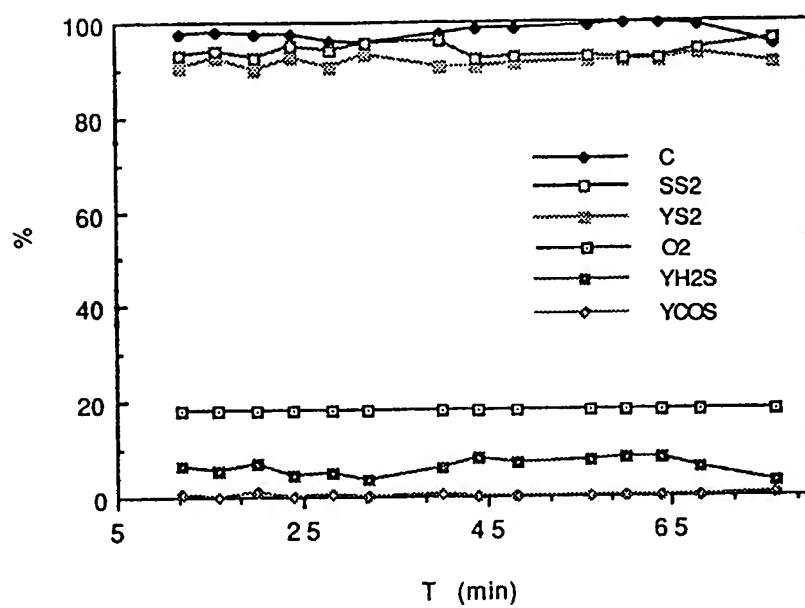


TABLE 29



INTERNATIONAL SEARCH REPORT

International application No.
PCT/US99/00848

A. CLASSIFICATION OF SUBJECT MATTER

IPC(6) : B 01 J 20/34, 38/72, 27/02, 27/055, 27/047, 27/051

US CL : 502/21, 216, 218, 219, 220

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 502/21, 216, 218, 219, 220

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	US 5,494,879 A (JIN et al) 27 February 1996, abstract, col. 6, lines 13-20, 39-42, 48-50, col. 8, lines 57-63, claims.	1-4
Y	US 4,491,639 A (HAPPEL et al) 01 January 1985, abstract, col. 1, lines 11-15, 30-40.	1-54
Y	US 4,825,013 A (QUARDERER et al) 25 April 1989, abstract, col. 3, lines 32-35, 50-54, col. 4, lines 5-19, 37-45.	5-12
A	US 3,864,459 A (STILES) 04 February 1975, abstract.	1-54
A	US 3,965,041 A (VAN KLINKEN et al) 22 June 1976, abstract.	1-54

☒ Further documents are listed in the continuation of Box C. ☐ See patent family annex.

* Special categories of cited documents:	*T* later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
A document defining the general state of the art which is not considered to be of particular relevance	*X* document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
E earlier document published on or after the international filing date	*Y* document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
L document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)	*G* document member of the same patent family
O document referring to an oral disclosure, use, exhibition or other means	
P document published prior to the international filing date but later than the priority date claimed	

Date of the actual completion of the international search

12 MARCH 1999

Date of mailing of the international search report

08 APR 1999

Name and mailing address of the ISA/US
Commissioner of Patents and Trademarks
Box PCT
Washington, D.C. 20231

Facsimile No. (703) 305-3230

Authorized officer

Cam Nguyen
CAM NGUYEN

Telephone No. (703) 308-0661

INTERNATIONAL SEARCH REPORT

International application No.
PCT/US99/00848

C (Continuation). DOCUMENTS CONSIDERED TO BE RELEVANT		
Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	US 4,626,339 A (CHIANELLI et al) 02 December 1986, abstract, col. 4, lines 28-36.	1-54
A	US 4,748,141 A (BAKER) 31 May 1988, abstract.	1-54
A	US 4,748,142 A (CHIANELLI et al) 31 May 1988, abstract.	1-54
A	US 4,831,060 A (STEVENS et al) 16 May 1989, abstract.	1-54
A	US 4,839,326 A (HALBERT et al) 13 June 1989, abstract.	1-54
A	US 4,882,360 A (STEVENS) 21 November 1989, abstract.	1-54
A	US 4,902,404 A (HO) 20 February 1990, abstract, col. 2, lines 35-40.	1-54